

# Energy Transition: An Optimization Approach for Green Hydrogen and Integration of HVO

The AIChE Netherlands/Belgium Section Meeting

Burcu Ekmekci

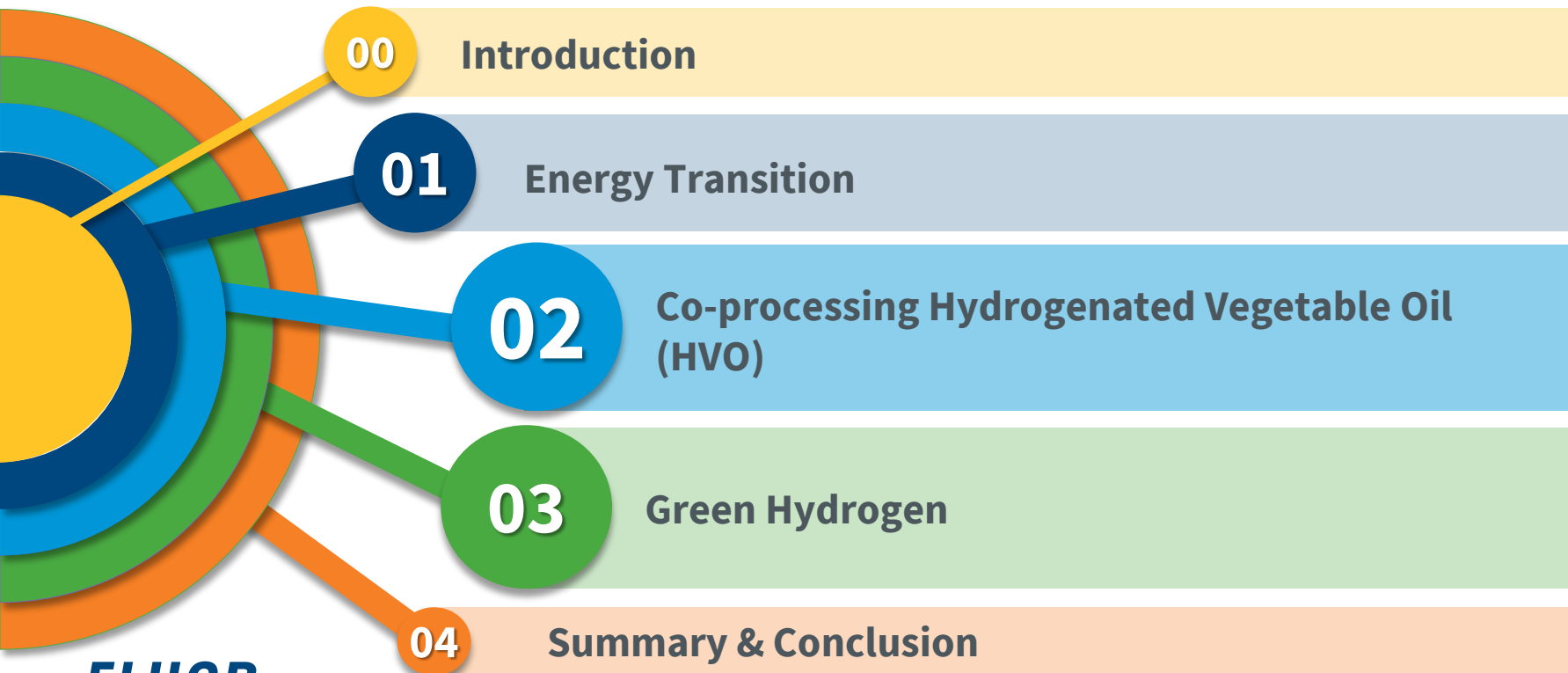
28 June 2022



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# Agenda

HVO  
H<sub>2</sub>



# It is NOT JUST Water

HVO  
H<sub>2</sub>

## ENERGY TRANSITION TECHNOLOGIES

This community is created to address the growing interest toward Energy Transition. Here, you'll find resources about Fluor's energy transition technologies and focus areas that can be used for business development efforts or for your own knowledge.



Click on the elements listed below to learn about how Fluor supports our Clients in their journey through Energy Transition

Carbon  
Capture

Electrification  
and Energy  
Efficiency

Energy  
Storage

Gasification

Green  
Chemicals  
and Plastics  
Recycling

Hydrogen  
Production,  
Storage and  
Transportation

Mining of High-  
Demand Metals

Modular  
Nuclear  
(NuScale)

Renewable  
Fuel  
Production

Renewable  
Power  
Generation &  
Integration with  
Production  
Facilities

Sustainability  
in Design  
and Project  
Delivery

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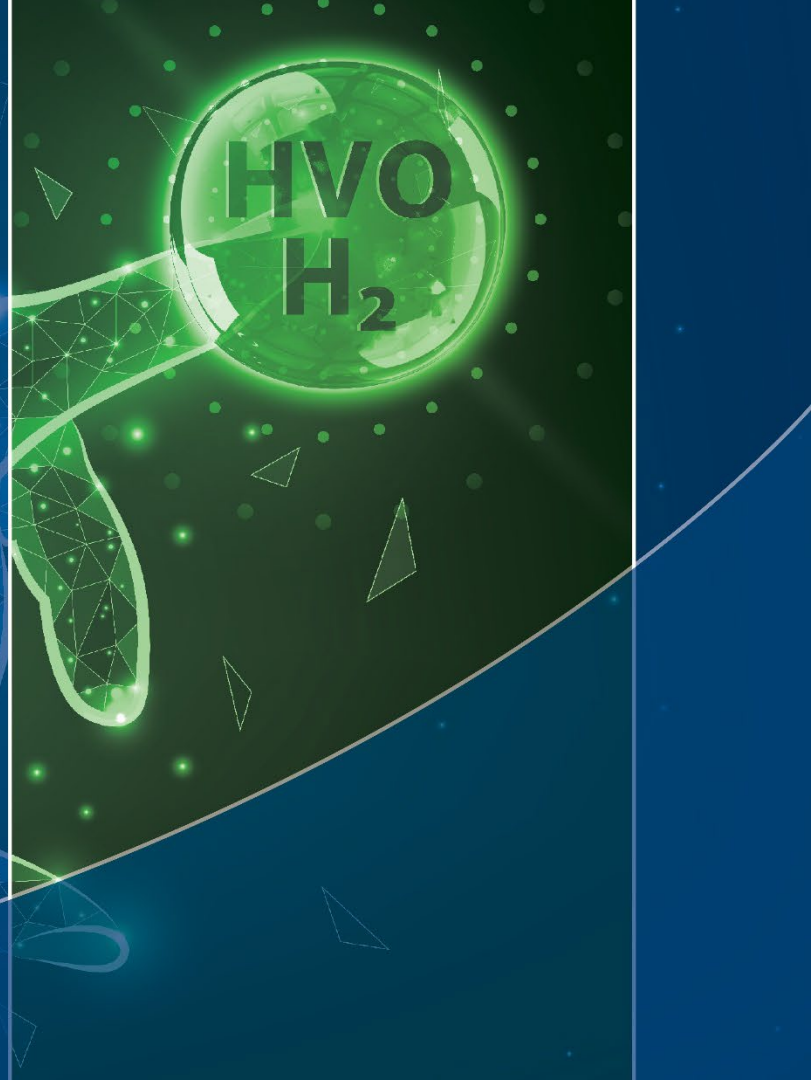
Water Group 2022

Burcu Ekmekci  
Fluor Fellow – Water and Wastewater  
Treatment



IT IS ~~NOT~~ WATER

HSE TOPIC



# What Happened?

HVO  
H<sub>2</sub>



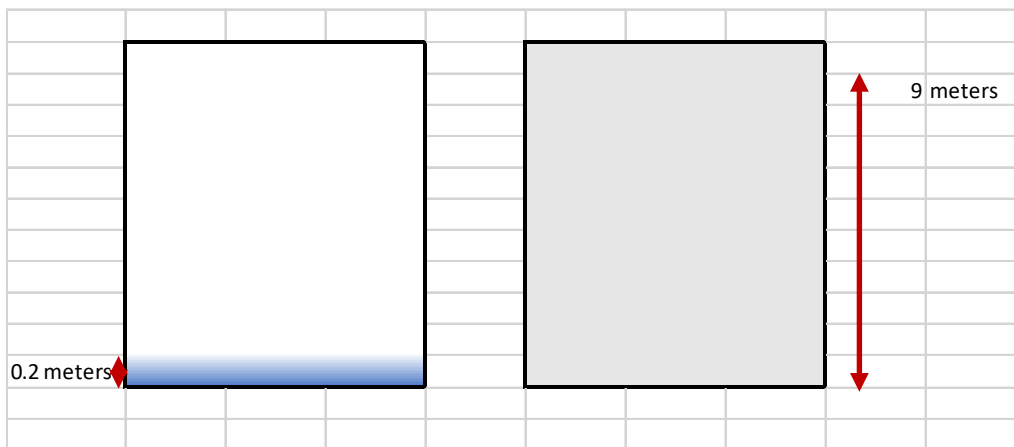
- ▶ The Omega Protein facility in Moss Point, Mississippi
- ▶ A tank explosion on July 28, 2014, killed a contract worker and severely injured another
  - The explosion blew the lid off the **30-foot/9-meters high tank**,
  - Fatally injuring a contract worker who was on top of the tank.
  - A second contract worker on the tank was severely injured.

# Why it happened?



The incident occurred during hot work on/near a tank containing

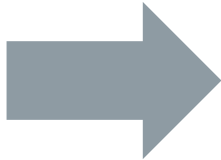
**8 inches / 20 cm** of a slurry of water



**Yes, only 20 cm of a slurry of water**

# How did it happen?

HVO  
H<sub>2</sub>

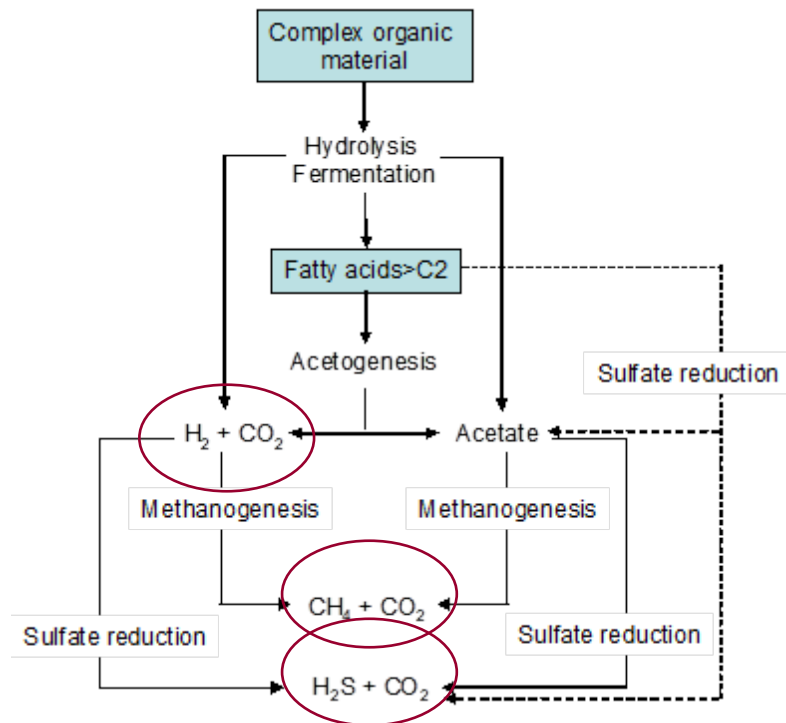
- ▶ The water inside of the storage tank had been thought to be nonhazardous
  - ▶ No combustible gas testing was done on the contents of the tank before the hot work commenced.
- 
- ▶ Signs of microbial activity in the samples
  - ▶ Presence of volatile fatty acids in the liquid samples
  - ▶ Off gassing of flammable methane and hydrogen sulfide



# How did it happen?



## Anaerobic Conversion



## Results in

- H<sub>2</sub>S Emission
- Hydrogen
- Methane
- Technical Expertise
  - Oxygen Transfer Rate
  - Tank Sizing
  - Understanding of Reaction Kinetics



# TAKE AWAYS – IT IS **NOT** JUST WATER



## IT IS **NOT** JUST WATER

- ▶ Extreme importance of careful hot work planning
- ▶ Danger of Hot Work on Tanks Containing Biological or Organic Material
- ▶ Hazard evaluation
- ▶ **Procedures for all storage tanks**
- ▶ Hot work dangers are not limited to the oil, gas, and chemical sectors where flammability hazards are commonplace

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Co-processing Hydrogenated Vegetable Oil  
(HVO)

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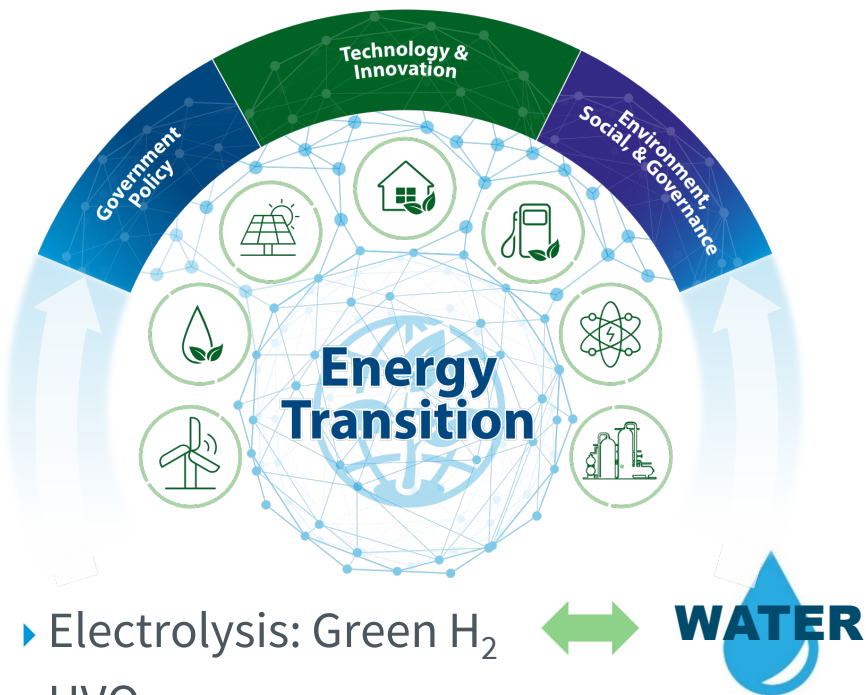
Green Hydrogen

04

Summary & Conclusion

# Energy Transition Linking with Water

HVO  
H<sub>2</sub>

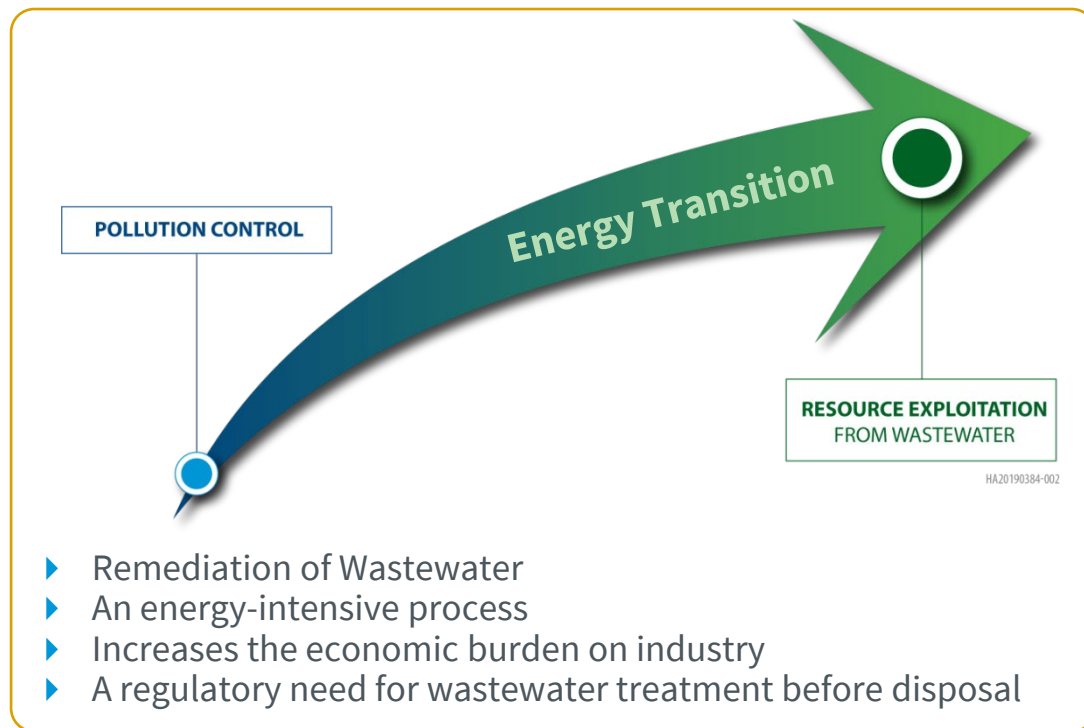


## Is water becoming “the new oil”?

- ▶ Large amount and stringent quality requirements
- ▶ Reuse of treated water effluent
- ▶ Integrated water management

# Integration of Water Solutions

HVO  
H<sub>2</sub>



- ▶ Water Reuse
- ▶ Produce value-added products
  - BioPlastic
- ▶ Product Recovery (Metals Li)
- ▶ Waste to Energy
  - Biogas
- ▶ Ultra Pure Water



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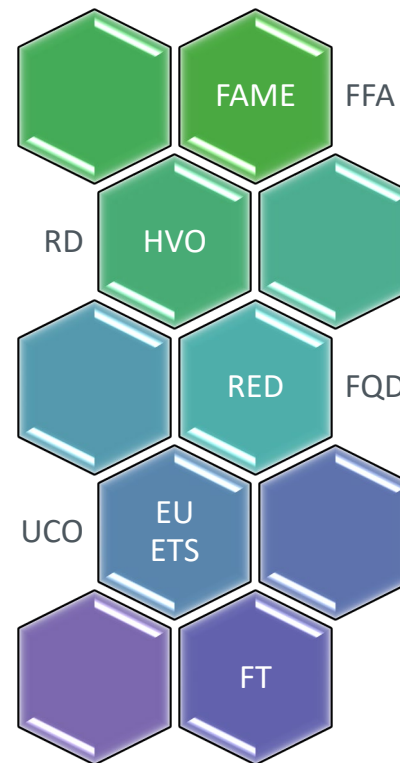
# Introduction and Background



HVO  
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## ► Well-known:

- Technology Selection
- Legislation
- Facility Match



# Introduction and Background



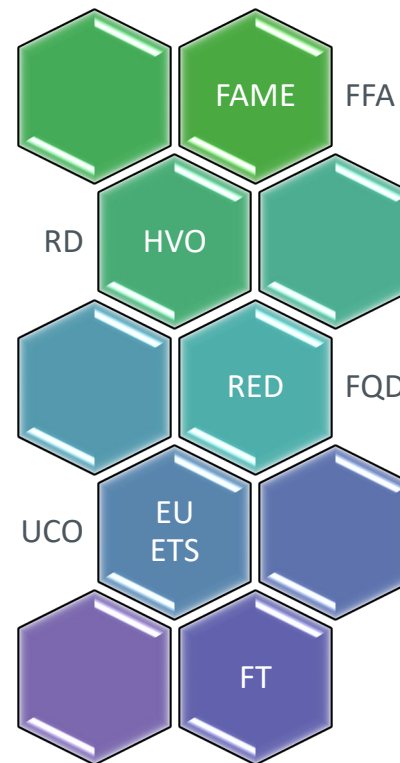
HVO  
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## ► Well-known:

- Technology Selection
- Legislation
- Facility Match

## ► How about:

- Implication of Utilities
- Implication of Environmental Permits

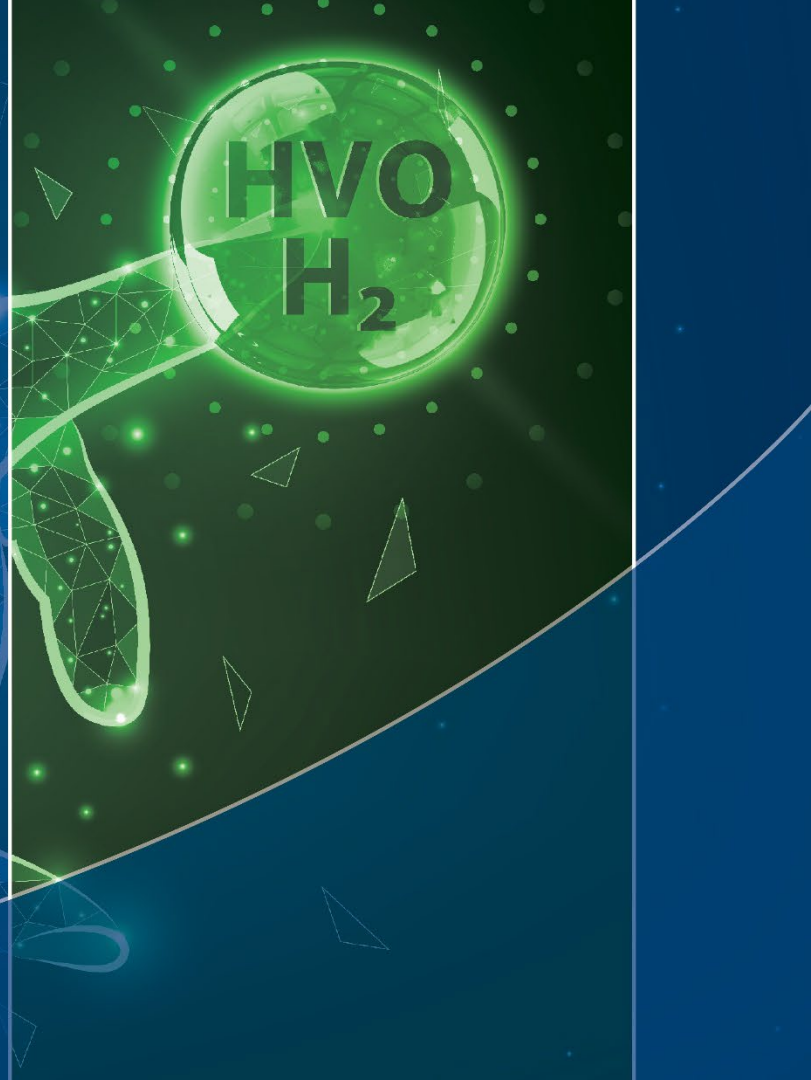


# Case Study



## Co-processing Hydrogenated Vegetable Oil (HVO)

- ▶ Utility Footprints
- ▶ Wastewater Treatment Plant Footprint





# Case Study Co-Processing



HVO  
H<sub>2</sub>



## ROUTE 1

Methanol and  
Caustic

Transesterification

**Biodiesel [FAME]**  
+ Glycerol

What is Co-Processing and how does it impact the existing process units

- Plant Oils
- Animal Fats
- Algae

## ROUTE 2

Hydrogen and  
Catalyst

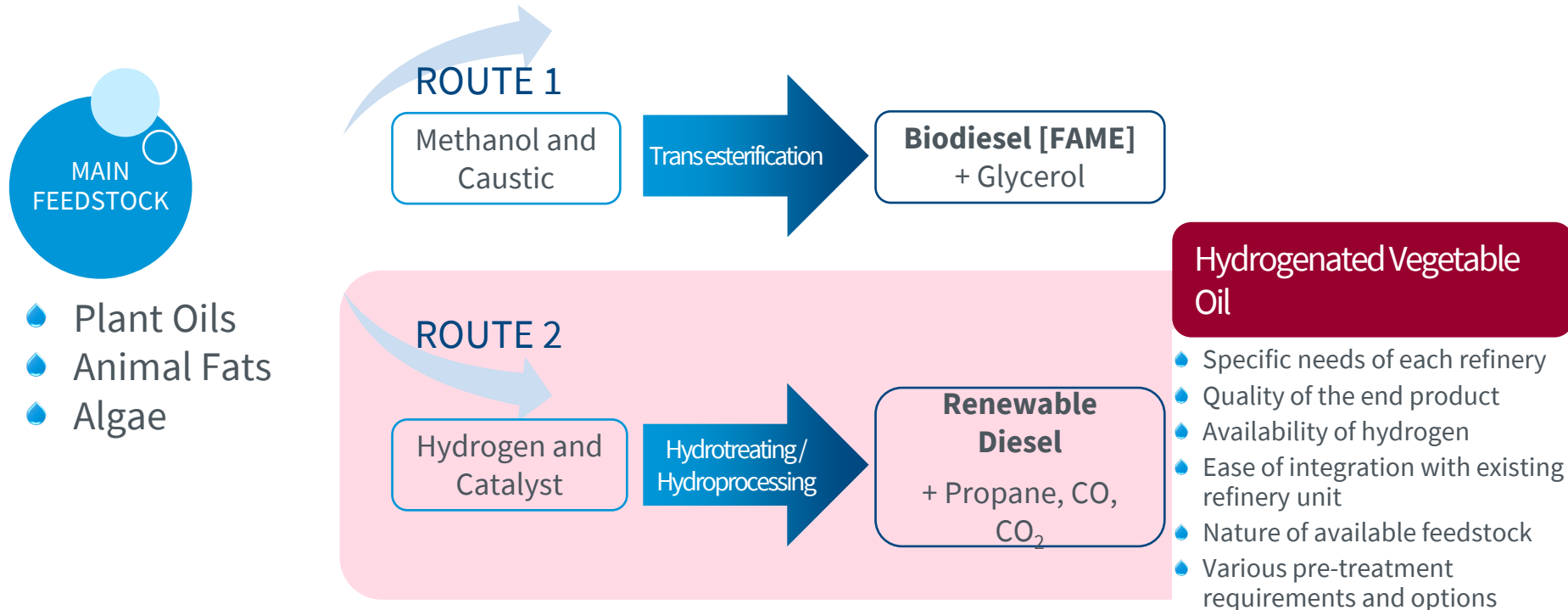
Hydrotreating/  
Hydroprocessing

**Renewable  
Diesel**  
+ Propane, CO,  
CO<sub>2</sub>

# Case Study Co-Processing



HVO  
H<sub>2</sub>

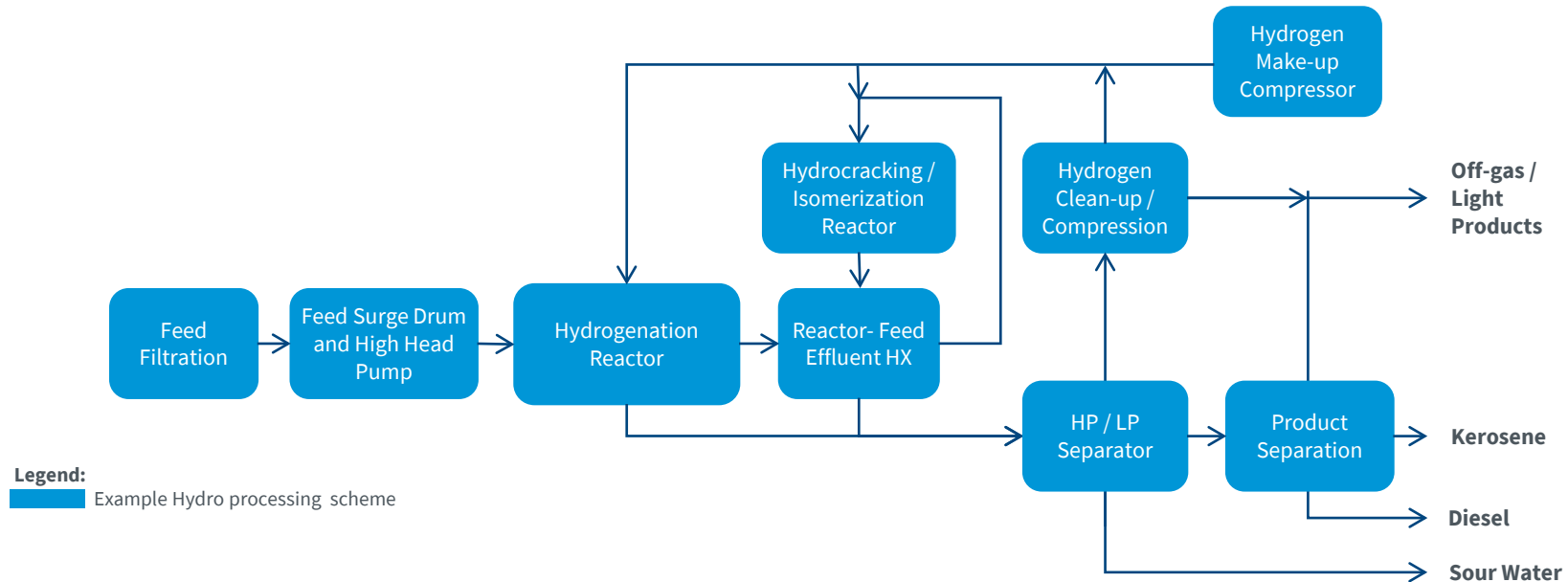


# Case Study

## Co-Processing Impacts on Utilities



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# Case Study

## Co-Processing Impacts on Utilities



HVO  
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### Pre-treatment:

- Characteristics of feedstocks
  - Alkali metals, phospholipids etc.

### Higher Exothermic:

- Provision of Quench gas lines and distributors
- Surge lines

Vegetable  
Oils Animal  
Fats Greases

Pre-treatment

Feed  
Filtration

Feed Surge Drum  
and High Head  
Pump

Hydrogenation/  
Decarboxylation/  
Deoxygenation  
Reactor

Hydrocracking /  
Isomerization  
Reactor

Reactor- Feed  
Effluent HX

Hydrogen  
Clean-up /  
Compression

Hydrogen  
Make-up  
Compressor

Off-gas /  
Light  
Products

HP / LP  
Separator

Product  
Separation

Renewable Jet

Renewable  
Diesel

Sour Water

Waste Water

### Legend:

- Example Hydro processing scheme
- Co-processing Add-ons



HDO could be existing or  
existing supplemented with an  
additional reactor.

### IMPACTS

- New Waste Water Stream
- Increased Sour Water Production

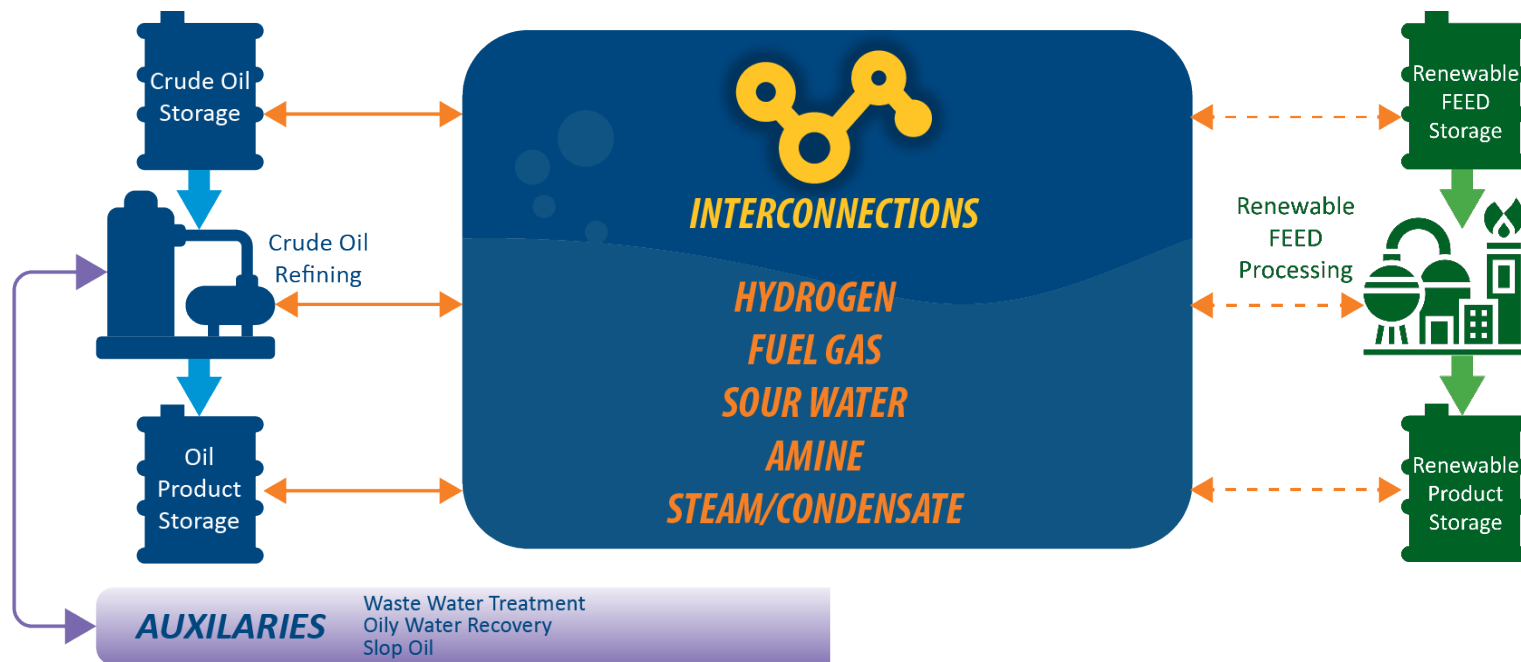


# Case Study

## Utility Footprints



HVO  
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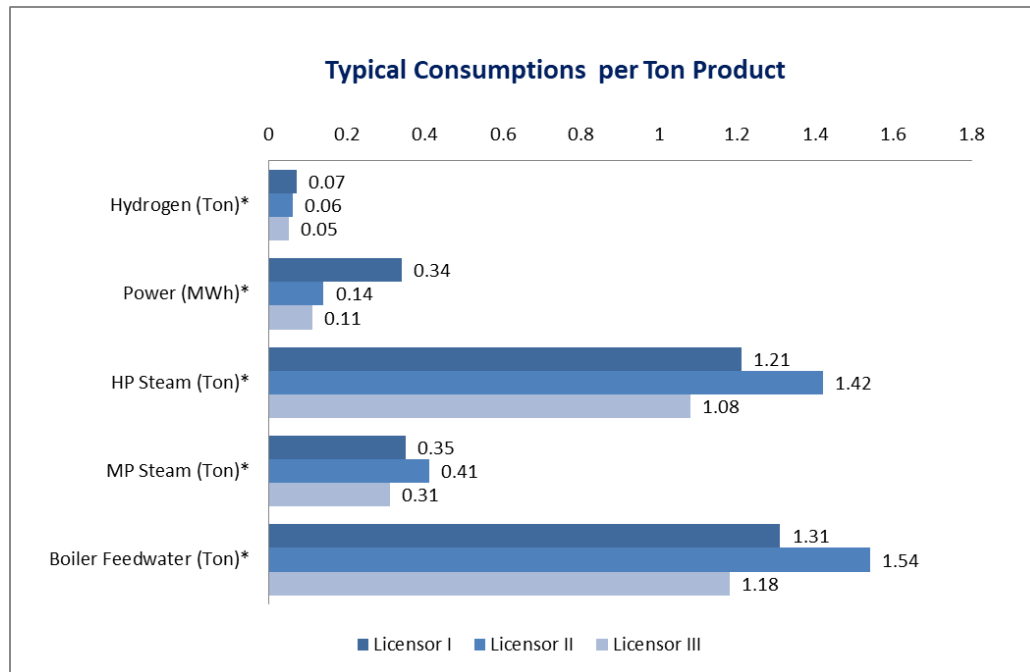
# Case Study

## Utility Footprints



HVO  
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- ▶ Quick Scan for the existing utility capacities
- ▶ Main Differences Power Consumption and Boiler Feedwater



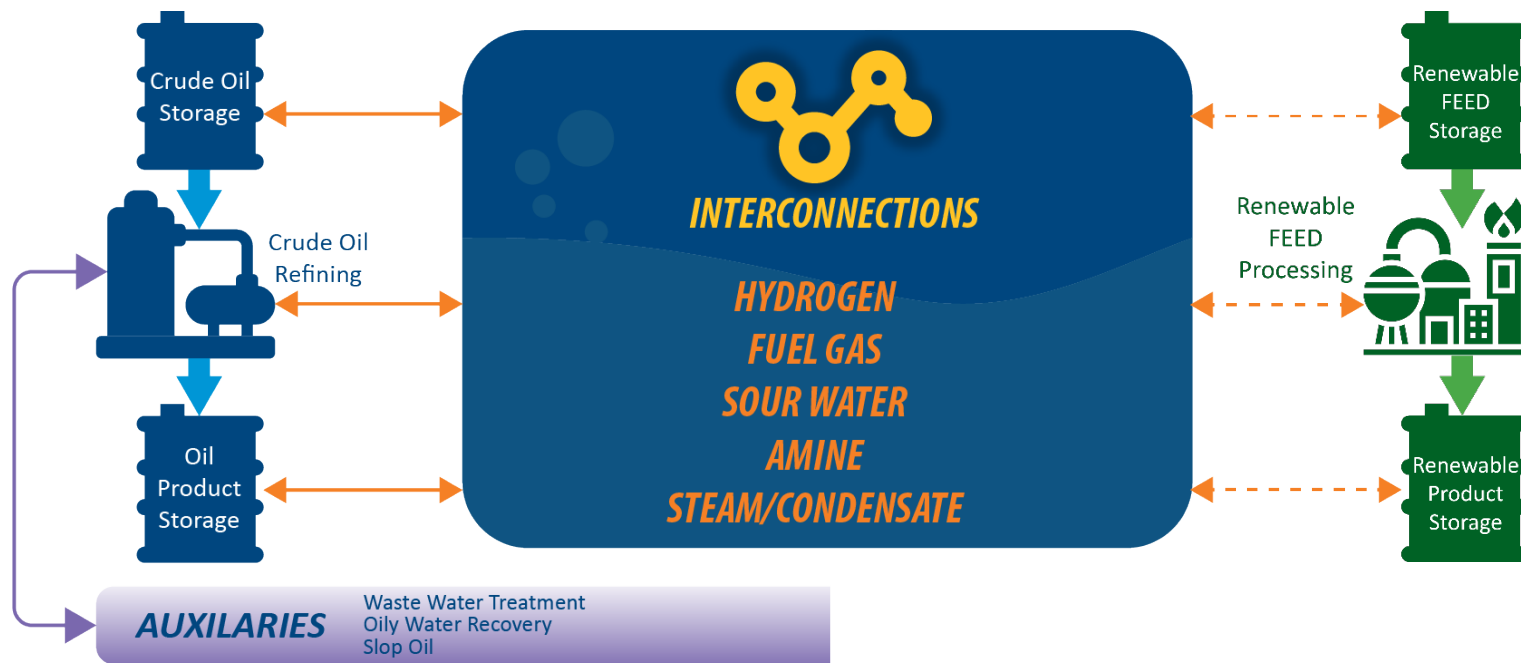
\*Data Source: Nexant Bio renewable Insights: Non-Ester Renewable Diesel, September 2019.  
UOP Ecofining, Haldor Topsøe Hydroflex, Neste NeXBT

# Case Study

## Utility Footprints



HVO  
H<sub>2</sub>



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# Case Study

## Utility Footprints



HVO  
H<sub>2</sub>



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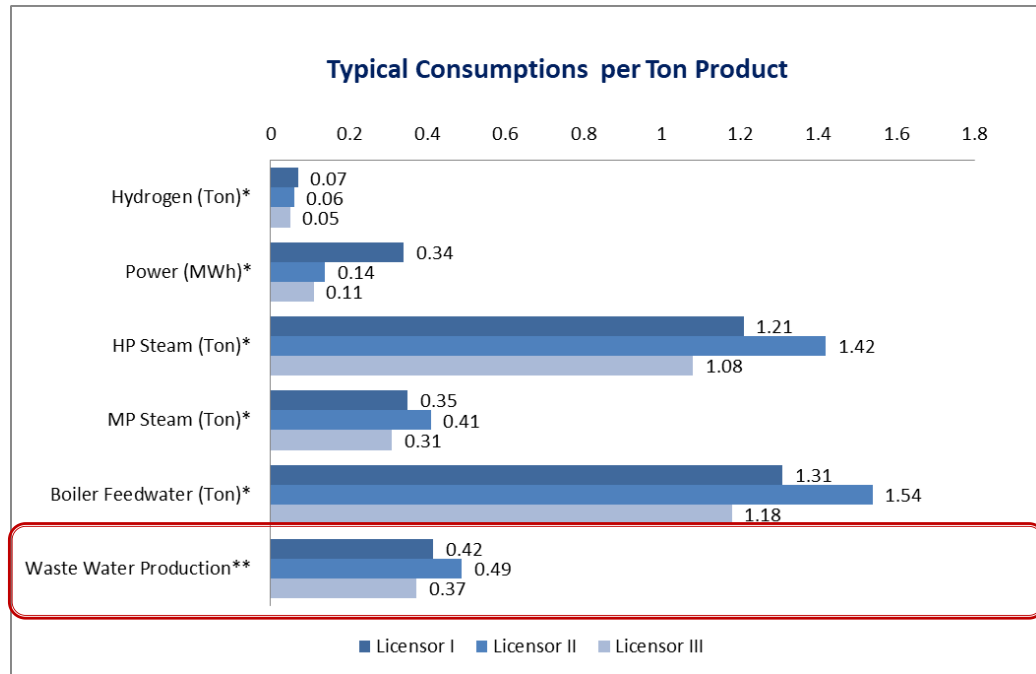
# Case Study

## Utility Footprints



HVO  
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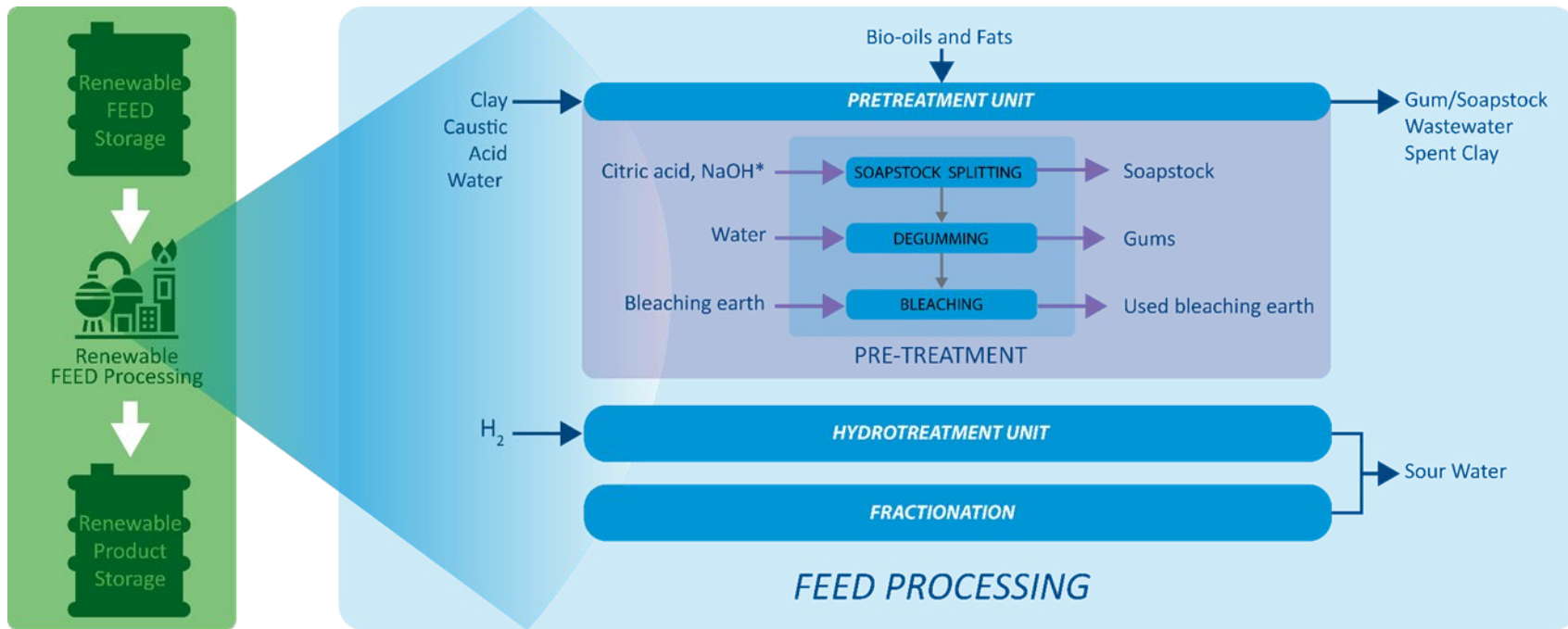
- ▶ Quick Scan for the existing utility capacities
- ▶ Main Differences Power Consumption and Boiler Feedwater
- ▶ The wastewater originated from the processing at least 10 – 30 % of the feed flow
  - ~ 10% for pre-treatment
  - ~ 20% for sour water draw



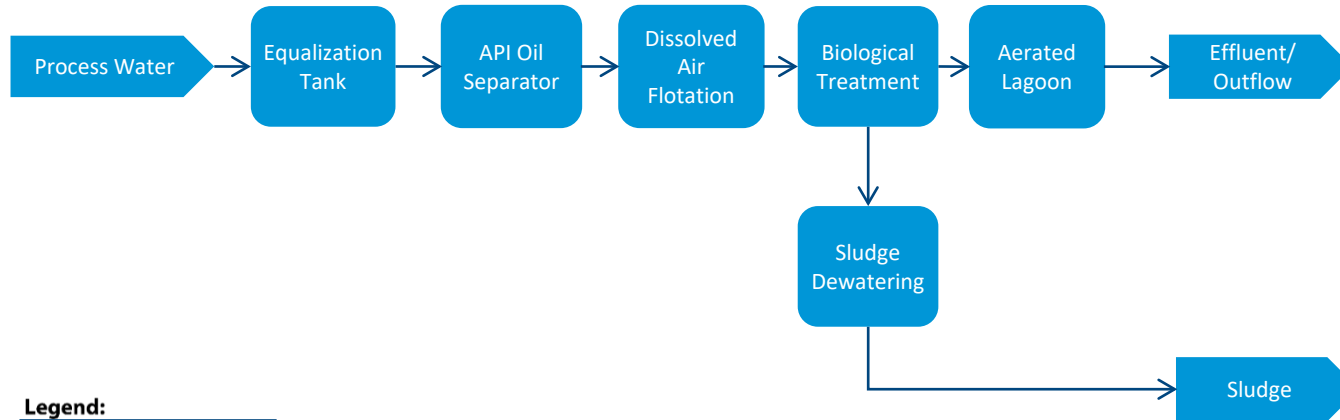
\*Data Source: Nexant Bio renewable Insights: Non-Ester Renewable Diesel, September 2019.

UOP Ecofining, Haldor Topsøe Hydroflex, Neste NeXBT

\*\* in-house Information



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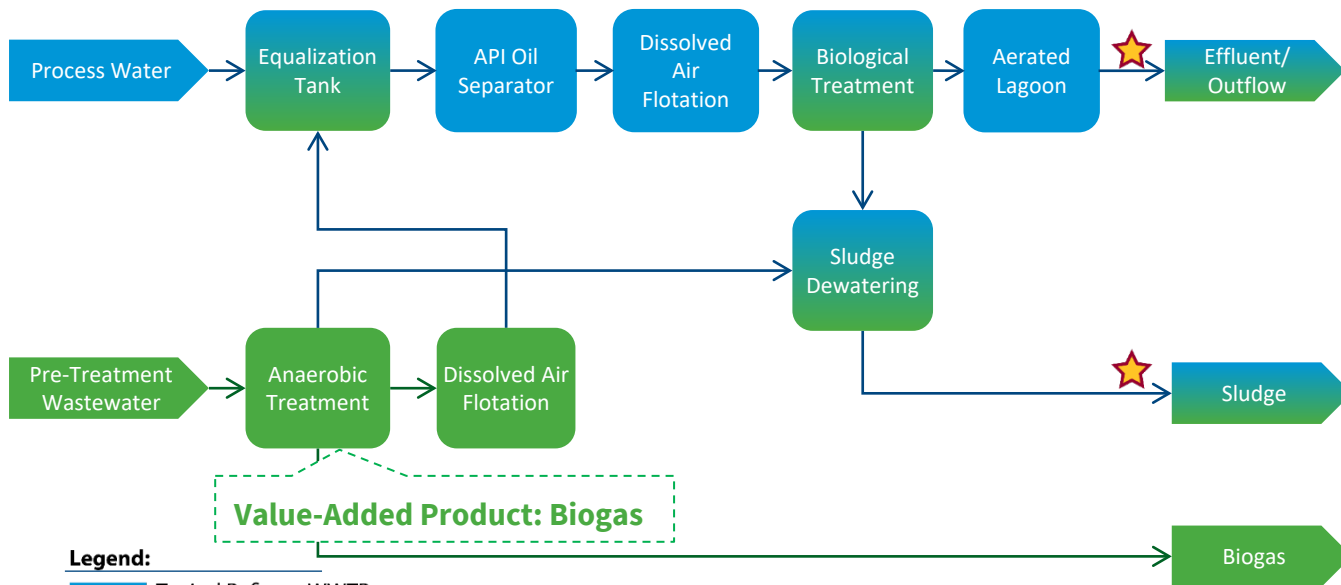


**Legend:**

Typical Refinery WWTP

**ABBREVIATION:**

API : American Petroleum Institute

**Legend:**

- Typical Refinery WWTP
- Additional Units for HVO
- ★ Permit Boundaries

**Additional Required Units:**

- Anaerobic Treatment
- Dissolved Air Flotation (DAF)
- Odor Removal Unit (optional)

**Modified Units:**

- Equalization Tank
- Biological Treatment
  - Additional Nitrogen and Phosphorus Removal (subject to permit discussion)
- Sludge Dewatering

# RECAP: HVO Water and Wastewater

HVO  
H<sub>2</sub>



Consider increasing market demand in Co-processing



Diligent approach to Process Technology Selection and full integration

**There are some “special “ aspects that can create some unexpected surprises !!!**



Foresee the implications on utilities plus impacts **Cannot be fixed in the process, should be taken care of in the downstream units**



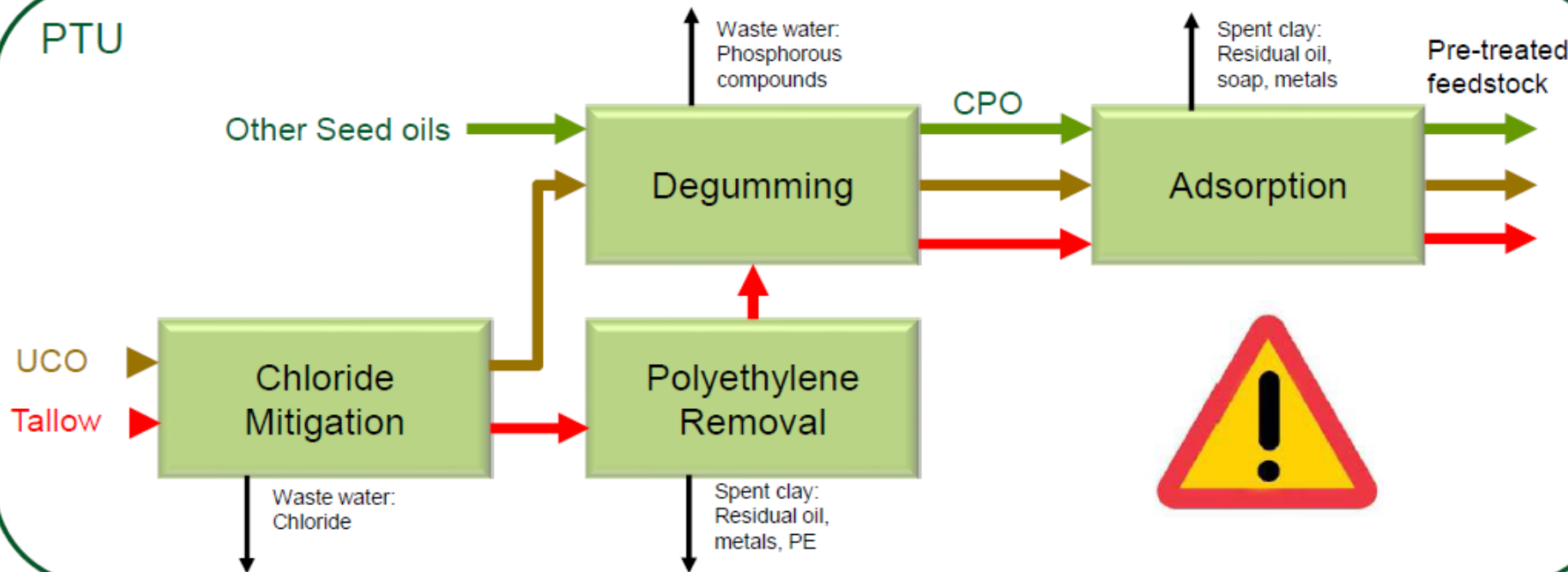
Be conscious on Wastewater Treatment and permits. **Trouble in permitting might also impact process and production**



# Bio feedstock

HVO  
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PTU



[www.alfalaval.com](http://www.alfalaval.com)

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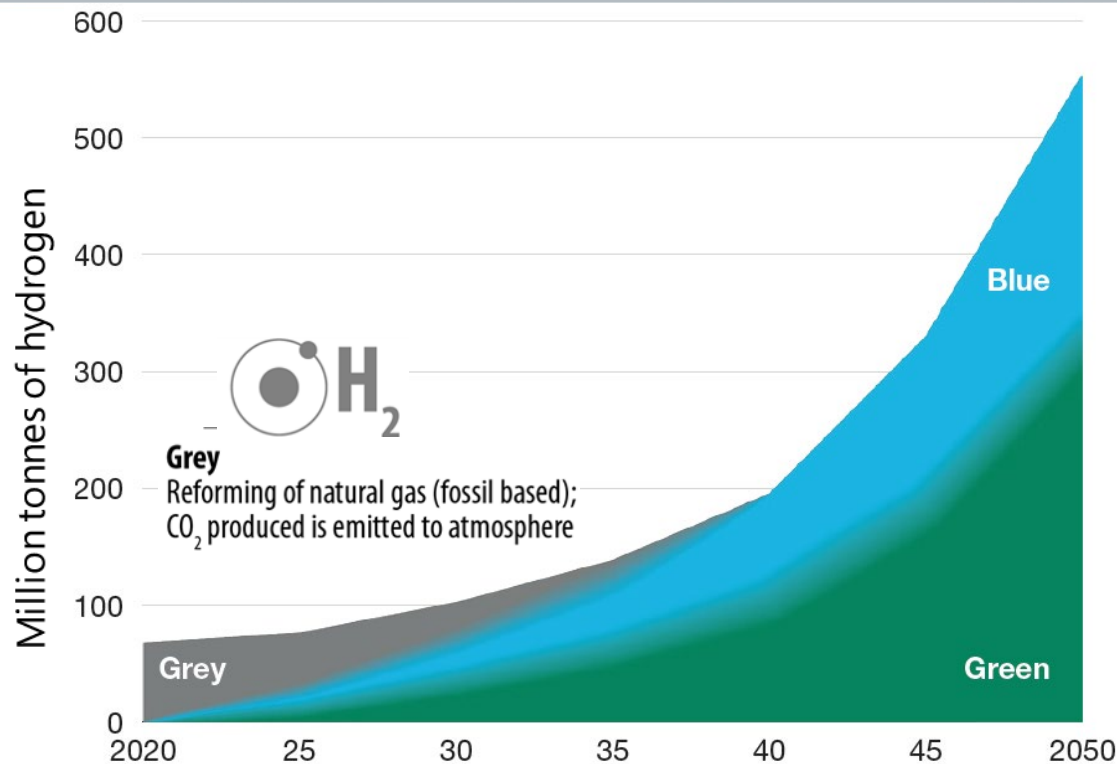
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Green Hydrogen

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Summary & Conclusion

# The Trending Green Hydrogen Global Production



**Grey**

Reforming of natural gas (fossil based);  
CO<sub>2</sub> produced is emitted to atmosphere



**Blue**

Reforming of natural gas (fossil based);  
CO<sub>2</sub> produced is captured and stored

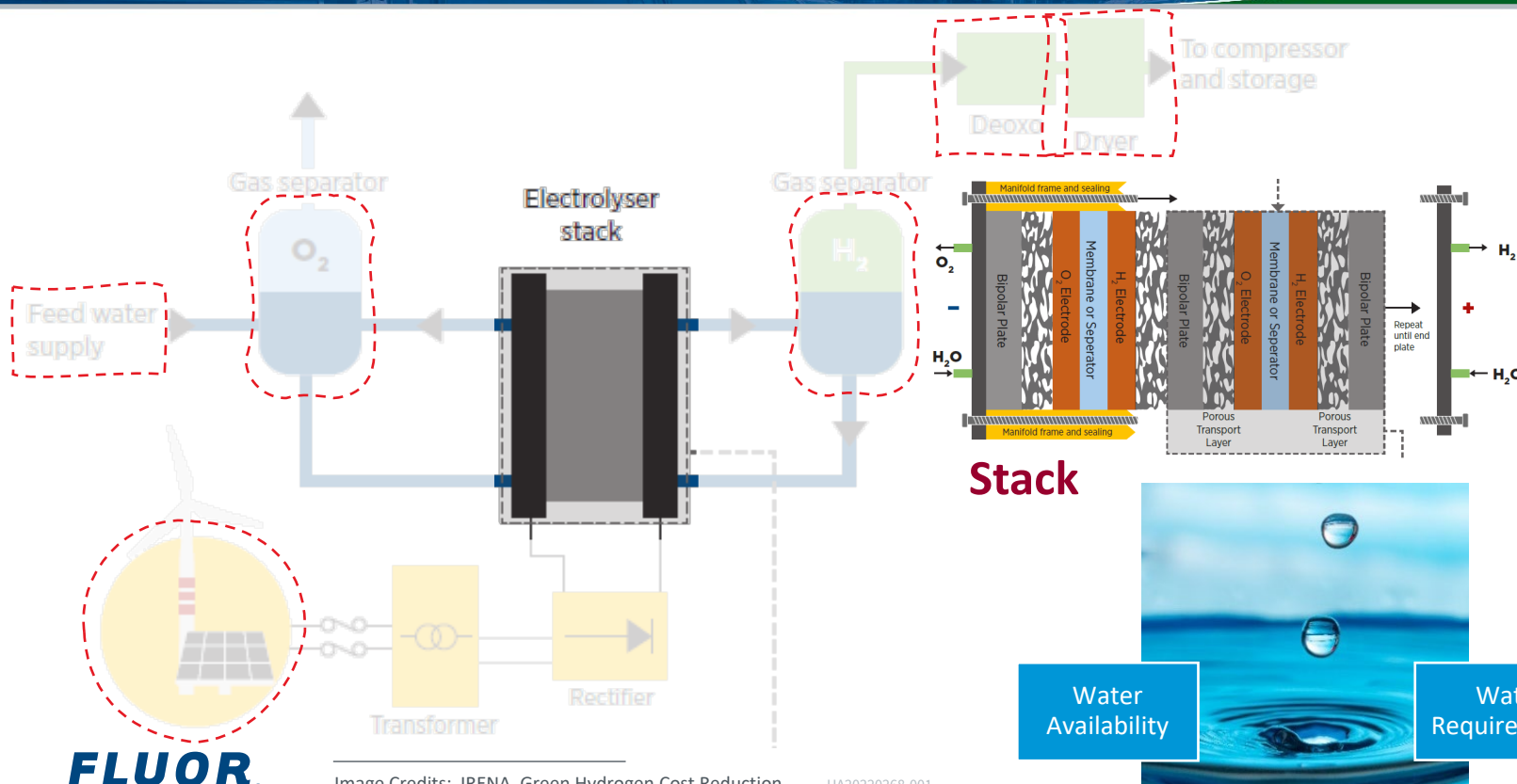


**Green**

Electrolysis of water; electricity  
only from renewable sources  
(no CO<sub>2</sub> production)

# Electrolysis Technology Working Principle

HVO  
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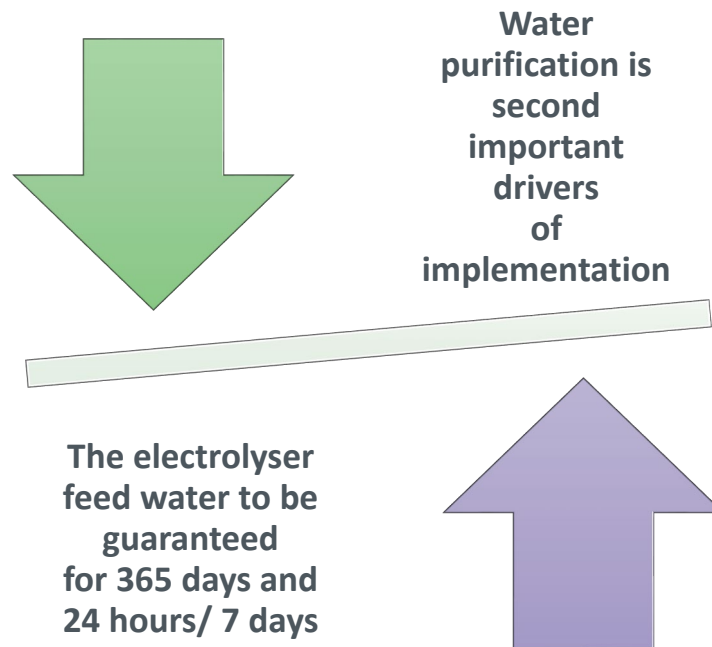
Image Credits: IRENA, Green Hydrogen Cost Reduction

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# Green Hydrogen



- ▶ Potential locations, hydrogen demand and plot sizes for these facilities
- ▶ System integration regarding infrastructure connections
- ▶ Availability of water and co-siting opportunities





# GW Scale Green Hydrogen Facilities



## Proposed GW Locations

## Water Infrastructure

## WW Treatment

- ▶ 5 industrial clusters
- ▶ A total of 22 locations are identified and available space and infrastructure have been evaluated.

All locations across the five regions;

- ▶ No existing nor any projected facility that can provide the demin water demand of around 200m<sup>3</sup>/h and quality required for the GW electrolyser

<https://rhk.maps.arcgis.com/apps/webappviewer/index.html?id=d94d70425c6b4c6f88a8143eda028d11>  
Source: Hydrohub: Integration of Hydrohub GigaWatt Electrolysis Facilities in Five Industrial Clusters in The Netherlands

# Feed Water Requirement in Electrolysis

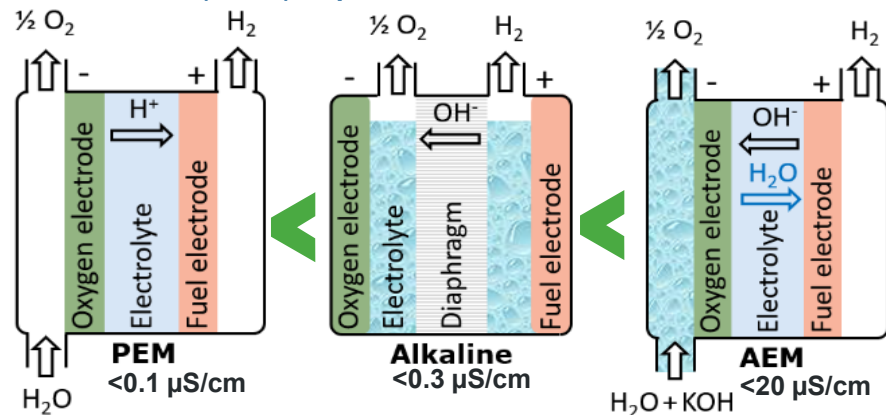
HVO  
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## Water

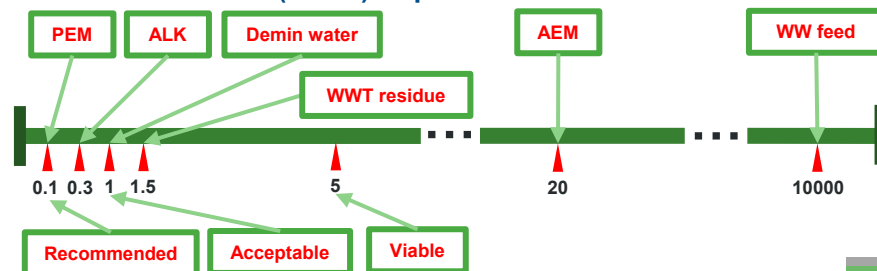
- ▶ **Low conductivity:  $<1 \mu\text{S}/\text{cm}$  is acceptable, although  $<0.1 \mu\text{S}/\text{cm}$  is recommended. Up to  $5 \mu\text{S}/\text{cm}$  may be viable.** At these low cond., individual component specs are less important.
- ▶ Residuals from the water treatment process is starting point. Treat WW\*:  **$1\sim 1.5 \mu\text{S}/\text{cm}$** .
- ▶ Extensive demineralization required. Demin water:  **$<1 \mu\text{S}/\text{cm}$** .
- ▶ The PEM water supply requires lower cond. ( **$<0.1 \mu\text{S}/\text{cm}$** ) than alkaline process water ( **$<0.2$  or  $<0.3\text{-}5 \mu\text{S}/\text{cm}$** ); AEM licensor indicates up to  **$20 \mu\text{S}/\text{cm}$** .

\* PO/TBA/POSM facility WWT unit effluent

Water (cond.) requirements for PEM, Alkaline, AEM:



Water (cond.) requirements overview



# Industrial Water Grade System

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Water Type Specifications as defined by ASTM D1193-91	Type I	Type II	Type III	Type IV
Electrical conductivity, max., $\mu\text{S}/\text{cm}$ at 298 K (25°C)	0.056	1.0	0.25	5.0
Electrical resistivity, min., MV cm at 298 K (25°C)	18	1.0	4.0	0.2
pH at 298 K (25°C)	*	*	*	5.0 to 8.0
Total organic carbon (TOC), max, $\mu\text{g}/\text{L}$	50	50	200	No limit
Sodium, max, $\mu\text{g}/\text{L}$	1	5	10	50
Chlorides, max, $\mu\text{g}/\text{L}$	1	5	10	50
Total silica, max, $\mu\text{g}/\text{L}$	3	3	500	No limit
Microbiological contamination – When bacterial levels need to be controlled, reagent grade types should be further classified as follows:	Type A	Type B	Type C	
Maximum heterotrophic bacteria count	10/1000 mL	10/100 mL	100/10 mL	
Endotoxin, EU/ml	<0.03	0.25	N/A	

\* The measurement of pH in Type I, II, and III reagent waters has been eliminated from this specification because these grades water do not contain consistent in sufficient quality to significantly affect the pH.

## Type I

- ▶ Ultrapure with a resistivity of  $>18 \text{ M}\Omega \text{ cm}$
- ▶ Required for analytical labs
- ▶ Applications include HPLC, gas chromatography, cell culturing, tissue culturing, mass spectrometry and any endeavor involving trace elemental laboratory instruments

## Type III

- ▶ Resistivity of  $>4 \text{ M}\Omega \text{ cm}$
- ▶ Produced using Reverse Osmosis (RO) and removes 90-99% of contaminants
- ▶ Applications include glassware rinsing, media preparation, feedwater use and other non-critical laboratory applications

## Type II

- ▶ Resistivity of  $>1 \text{ M}\Omega \text{ cm}$
- ▶ Cleaner than Type III but not ultrapure
- ▶ Applications include electrochemistry, sample dilution, radioimmunoassay and media preparation

## Type IV

- ▶ Resistivity of  $200 \text{ K}\Omega \text{ cm}$
- ▶ Generally produced by RO
- ▶ Typically used as feedwater to a Type I or Type II deionized (DI) system

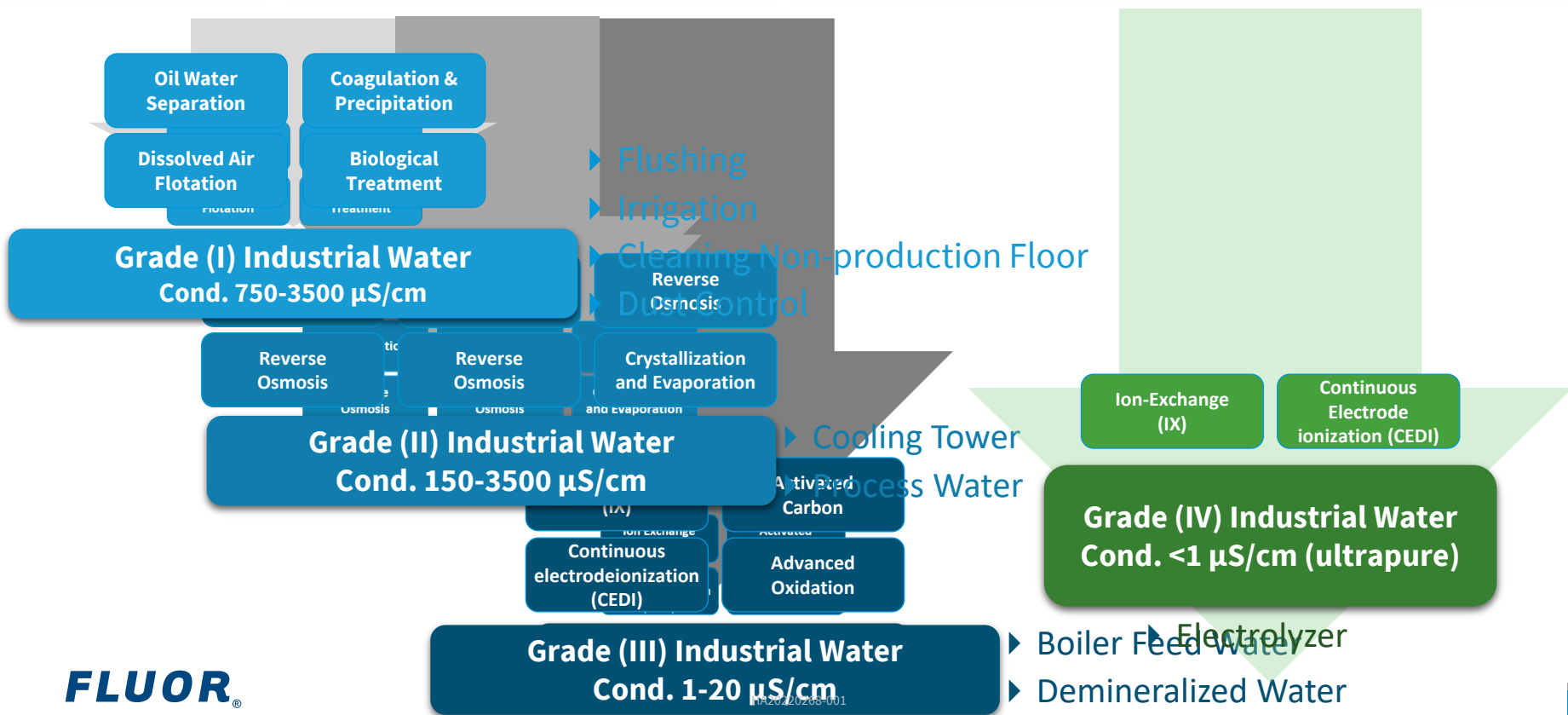
Water Quality Standard ASTM Type II

ISO 3696 Standard Grade II:ISO 3696:1987 Water for analytical laboratory use

[https://www.labconco.com/articles/water-type-difference#:~:text=Type%20I%20%2D%20Ultrapure%2C%20Type%20I,Total%20Organic%20Carbons%20\(TOC\).](https://www.labconco.com/articles/water-type-difference#:~:text=Type%20I%20%2D%20Ultrapure%2C%20Type%20I,Total%20Organic%20Carbons%20(TOC).)

# Industrial Water Grade System

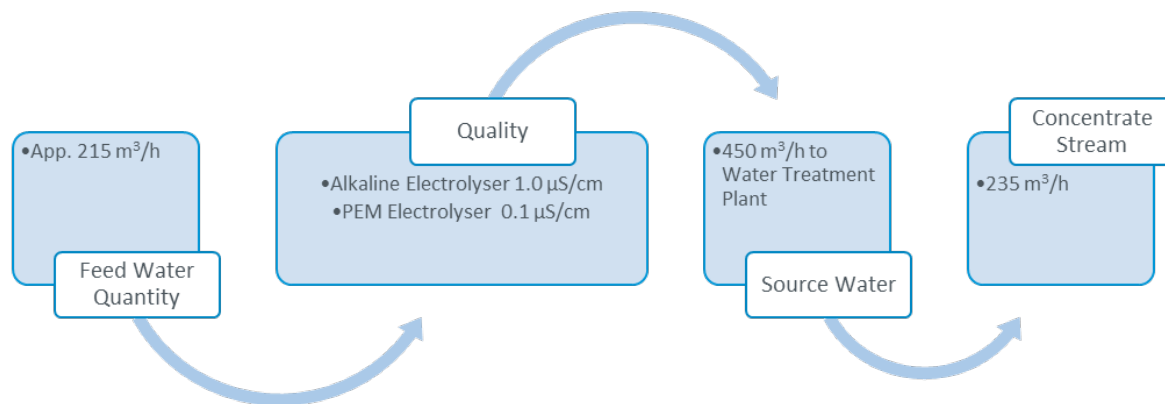
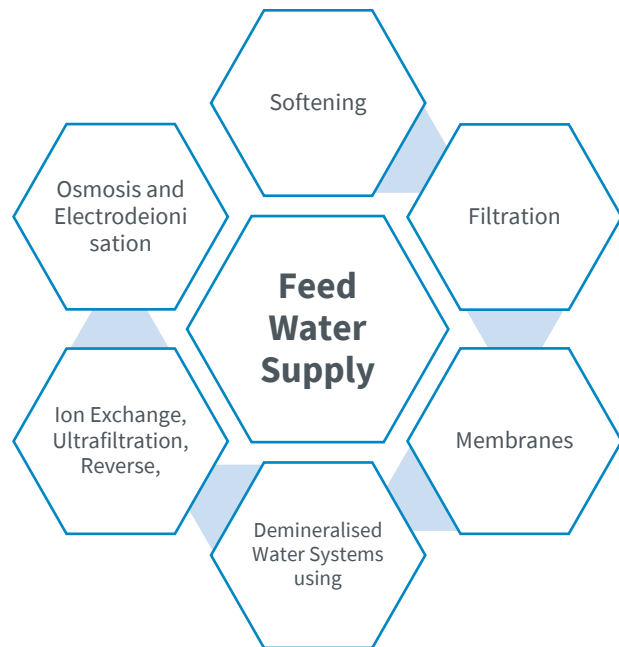
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# Feed Water Supply

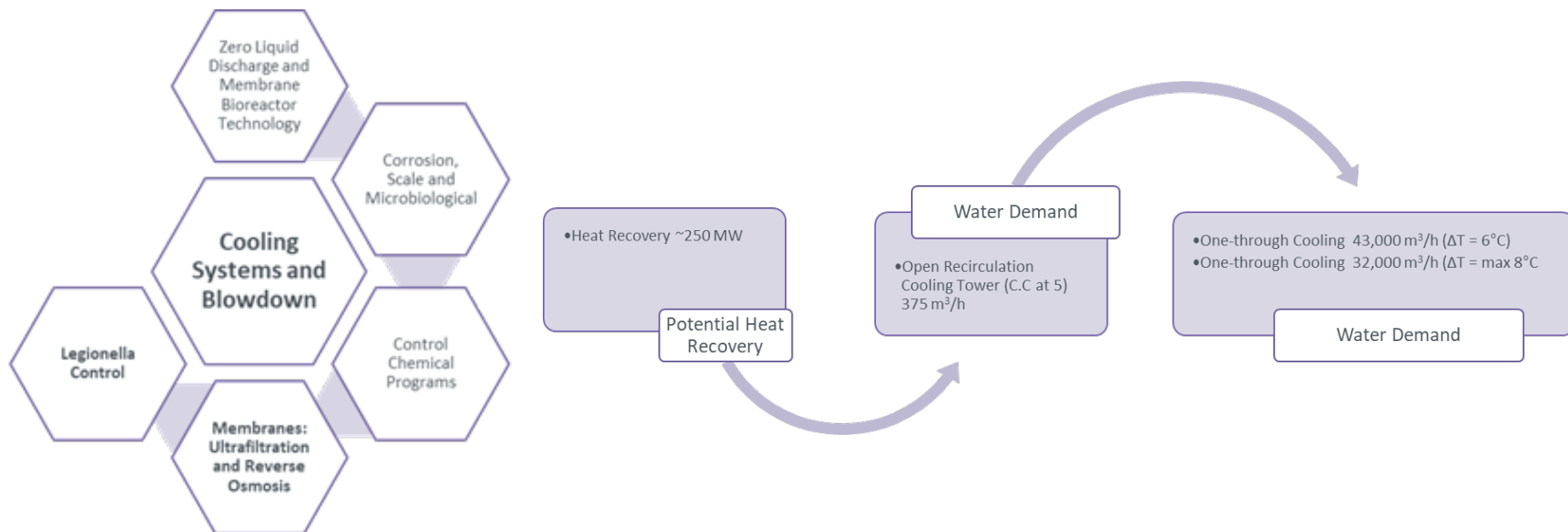
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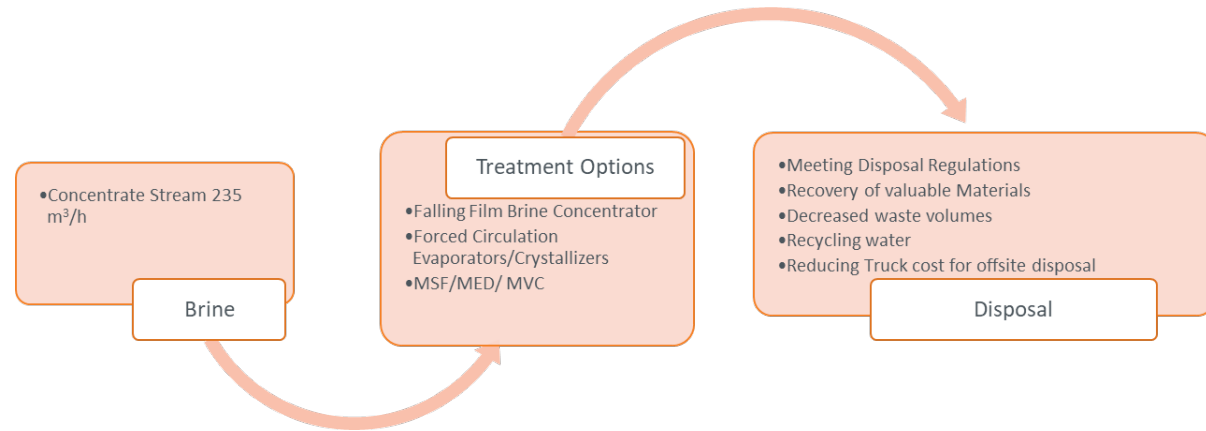
# Cooling Water Systems

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# Wastewater Treatment and Reuse

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# Technology Map

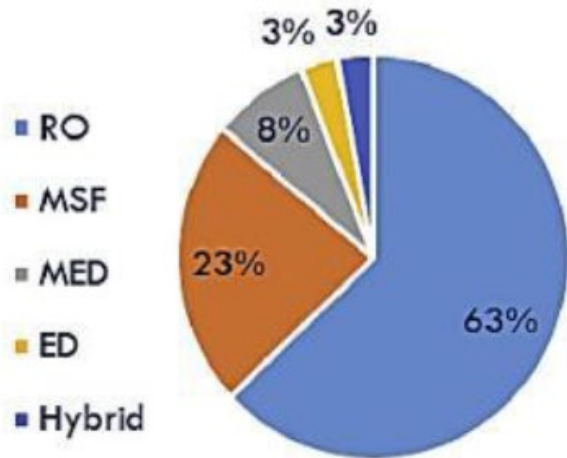


	Technology	ABBR	Type of Technology	Scale	Water Input	TRL Level (Current)	Output Water Quality [PPM]	Average Capacity [10 <sup>3</sup> m <sup>3</sup> /day]
1	Multi-Effect Distillation	MED	Evaporation and Condensation	Commercial	SW	9	10	0.6 - 30
2	Multi-Stages Flash	MSF	Evaporation and Condensation	Commercial	SW	9	10	50 to 70
3	Thermal Vapour Compression	TVC	Evaporation and Condensation	Commercial	SW	9	10	10 to 35
4	Mechanical Vapour Compression	MVC	Evaporation and Condensation	Commercial	SW	9	10	0.1 - 3
5	Saltwater Reverse Osmosis	SWRO	Filtration	Commercial	SW	9	400-500	1 - 627
6	Brackish Water Reverse Osmosis	BWRO	Filtration	Commercial	BW	9	200-500	Up to 98
7	Forward Osmosis	FO	Filtration	In development special application (hydration bags)	SW, BW	4		0.01 - 10
8	Nanofiltration	NF	Filtration	In development at dual stage unit	BW, SW Development	6		26.4 (ger)

# Technology Selection

HVO  
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## A Desalination by Technology

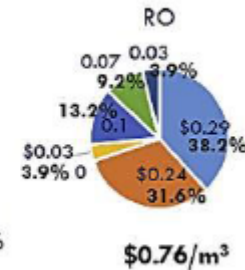
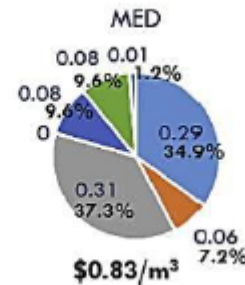


Energy Recovery Device (ERD)

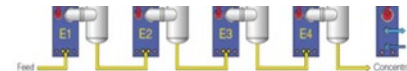
Source: Lenntech, 2018

## C

- Amortised capital cost
- Electrical energy
- Thermal energy
- Membranes
- Labor
- Chemicals
- Miscellaneous

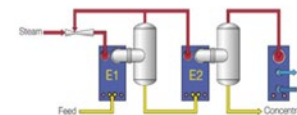


Steam or waste heat (hot water 90-95°C)



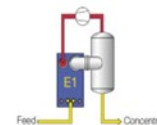
- TVR Thermo Vapour Recompression

Steam > 3-4 barg



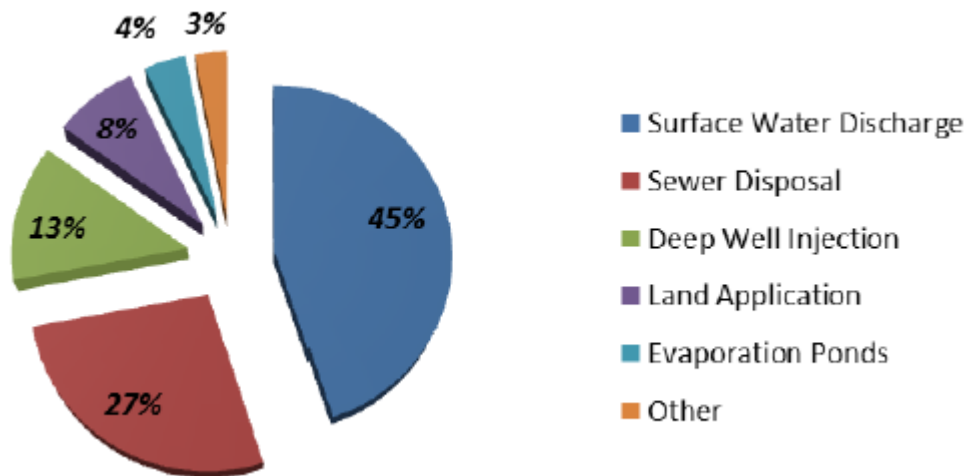
- MVR Mechanical Vapour Recompression

No steam required



# Brine Treatment

HVO  
H<sub>2</sub>



- ▶ Bench scale test
  - Physical properties
  - Boiling point elevation
  - Crystallization, fouling, concentration limits



#### MLD – Minimum Liquid Discharge

- Evaporator Only
- Effluent (residual waste) is Liquid
- < 40 wt% Total Solids (dissolved + crystals)
- Limit solids content to avoid plugging



#### ZLD – Zero Liquid Discharge

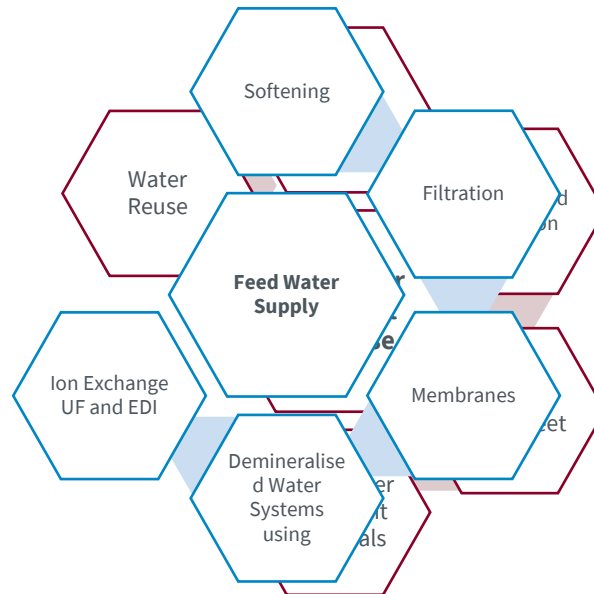
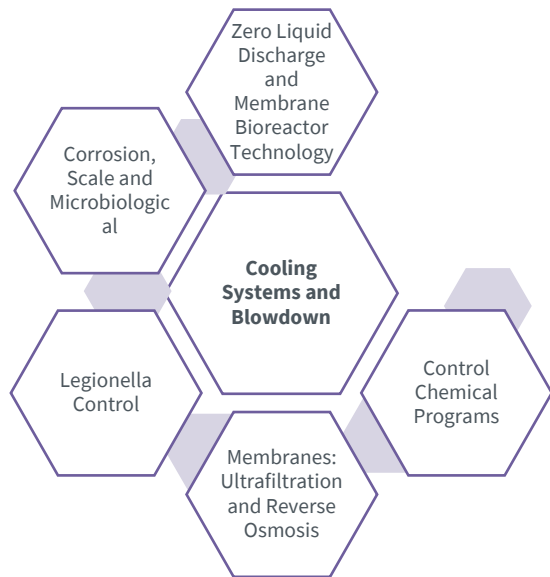
- Evaporator + Solids Dewatering (decanter centrifuge)
- Effluent (residual waste) is Solid
- Cake Dryness up to 85 wt% (no liquid water dripping)

Source: Lenntech, 2018



# An Integrated Water Management

HVO  
H<sub>2</sub>



# RECAP: Water for Green Hydrogen



- Global trends show that production of green hydrogen is replacing grey hydrogen.
- Electrolysis requires large amounts of water with stringent quality requirement i.e., in conductivity.
- Treated Effluent maybe be the starting point of electrolysis, with 1 uS/cm preferably.
- Alkaline electrolyser can handle water with higher conductivity values up to 5 uS/cm compared to PEM
- Integrated Water Management is crucial



RECAP

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# Summary & Conclusion



## Water is an integral part of energy transition




- ▶ Energy Transition Technologies gain great momentum and strong link with water.
- ▶ Definition of a higher grade of industrial water
- ▶ Product Recovery becoming important due to stringent water requirements
- ▶ Various wastewater treatment steps to recover different pollutants are required
- ▶ An integrated Water System is becoming more and more unavoidable
- ▶ Integrated Water Systems: Utilities system and wastewater system to be handled as one.



## FLUOR INTEGRATED WATER SOLUTIONS

### MINIMIZE AT SOURCE



-  Optimisation of production processes
-  Increase of efficiency
-  Not creating needless waste

### REUSE



-  Water Pinch Analysis
-  Lean Water Investment

### PRODUCE



-  Biorefinery Focus
-  Valorisation of Wastewater



# Questions?

HVO  
H<sub>2</sub>



# Contact Details



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## Thank You!

**FLUOR**<sup>®</sup>