



30th Annual European AIChE Seminar
**“Excellence in Operations, Workforce Engagement
and Human Factors”**

BASF Antwerp

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WHY? Workforce Involvement

- Sustainable knowledge management of process safety concepts within the manufacturing departments.
- Striving for “Excellence in Operations” by experience exchange – crossing plant borders into a “Technology Verbund”
- Bring Process Hazard Analysis to Full Potential by focus on further use as Training Instrument.

WHAT? Evaluation AS IS/ TO BE

- “AS IS” at BASF Antwerp
 - Hazard classification
 - Overview process safety studies
 - Overview scope & timing revisions
 - Process Safety management systems
 - Incident database
 - MOC procedure (SAP)
 - Maintenance & testing history (SAP)



Training at BASF

Knowledge of an installation can be obtained through a combination of:

- Theoretical training
 - Self-study guided by the VAPRO questionnaires
 - Courses organized by BASF
- Practical training
 - Training on the job
 - Simulator training
 - Start up of the installation
 - Manage disturbances in the process



WHAT? Evaluation AS IS / TO BE

- “TO BE” at BASF Antwerp
 - Higher involvement of operators in risk assessment
 - More reporting of near misses to validate next risk assessment
 - Avoid operational errors by broadening the knowledge basis of the process operators



HOW? PHA as training instrument

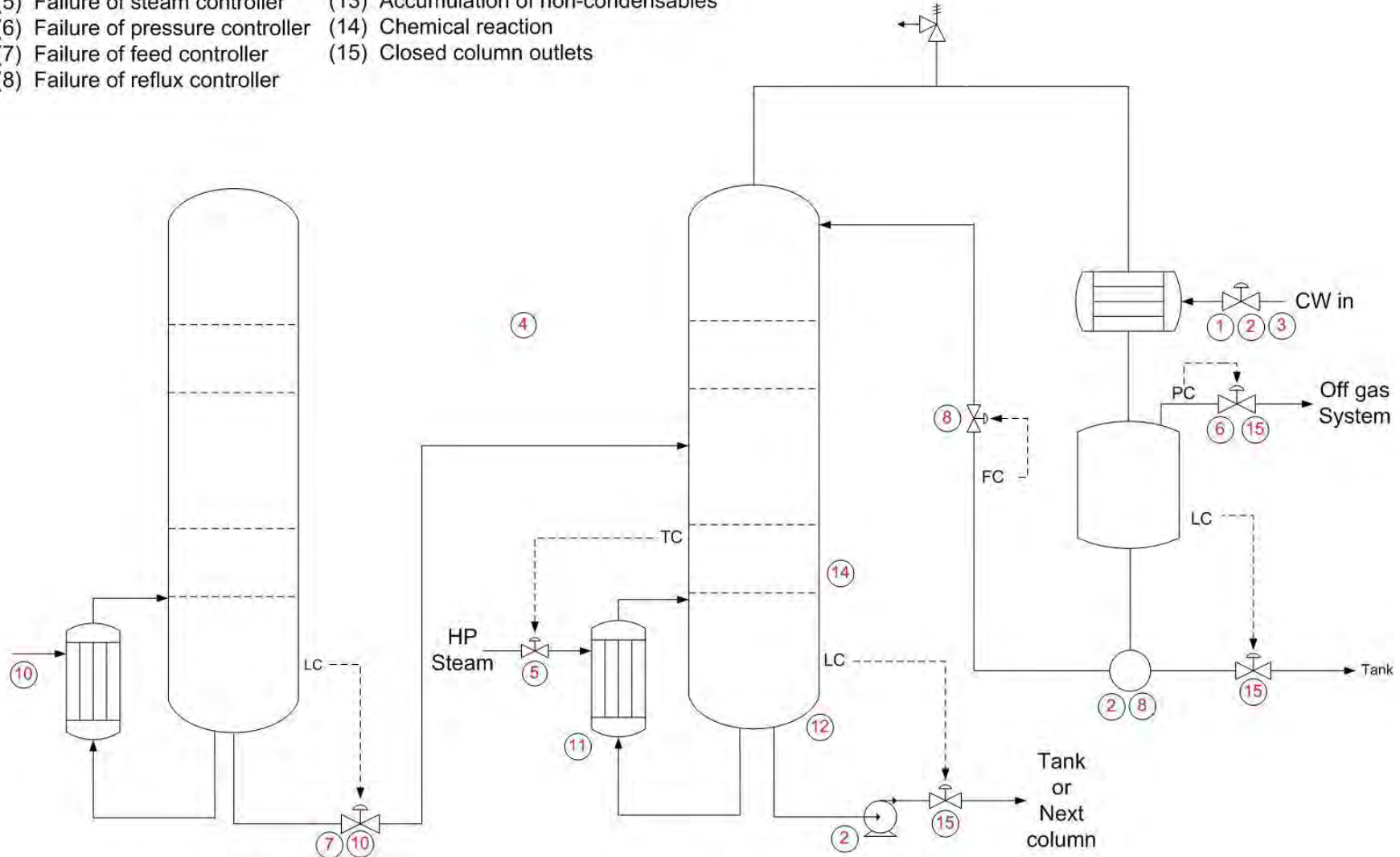
- Focus on further use as training instrument:
 - Use generic process units as basis for process safety philosophy.
 - Combine P&ID's in one overview diagram, representing only safety critical items.
 - Separate drawings for piping systems (recycle, off spec, start up , ... lines) can be very useful for shutdown and start up planning.
 - Expand process manual with an additional paragraph focusing solely on process safety and which summarizes result of risk assessment.

Example : Distillation Column

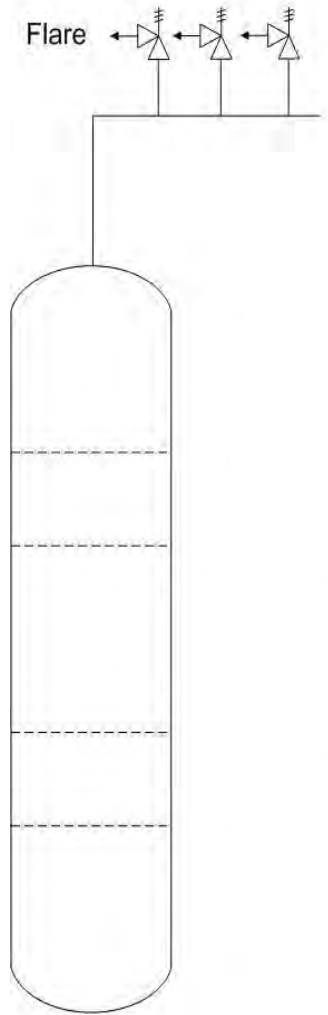
- Objective of distillation: separation of mixtures in pure components or different fractions.
- Technology is energy intensive as separation is based on gas / liquid interchange. Reboilers and condensers are used respectively for creating the gas and liquid flow.
- “Internals” in a distillation column will not be further discussed as the engineering of these is focused on a lower energy consumption and/or on an efficient separation.

Distillation Overpressure Relief

- | | |
|------------------------------------|---|
| (1) Loss of cooling | (9) Valve opening to an external source |
| (2) Loss of power | (10) Loss of heating upstream column |
| (3) Loss of steam | (11) Failure of exchanger |
| (4) Loss of instrument air | (12) Exterior fire |
| (5) Failure of steam controller | (13) Accumulation of non-condensables |
| (6) Failure of pressure controller | (14) Chemical reaction |
| (7) Failure of feed controller | (15) Closed column outlets |
| (8) Failure of reflux controller | |

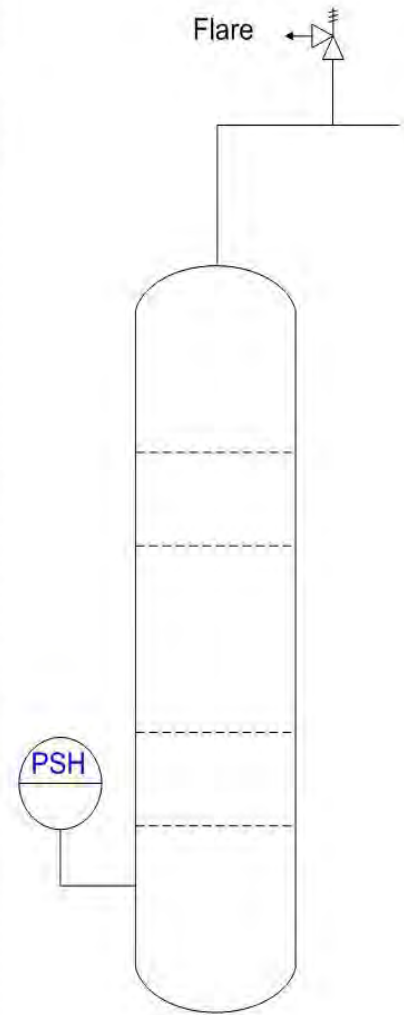


OVERPRESSURE PROTECTION DISTILLATION COLUMNS



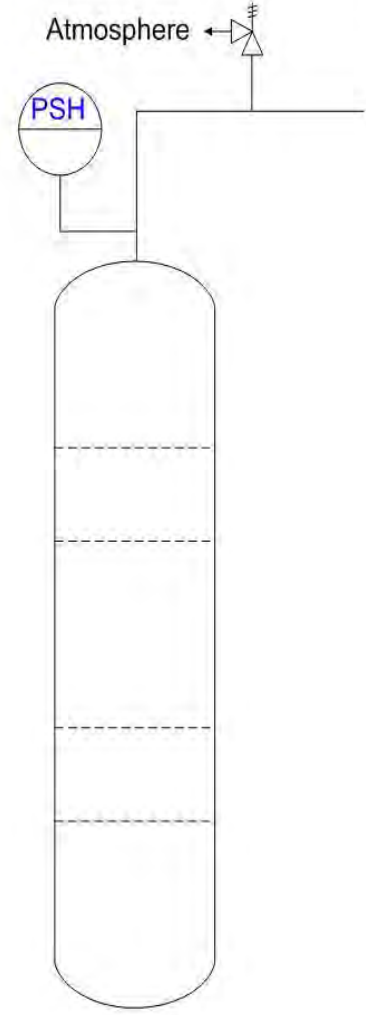
"OPEN"

Design
Relief valve



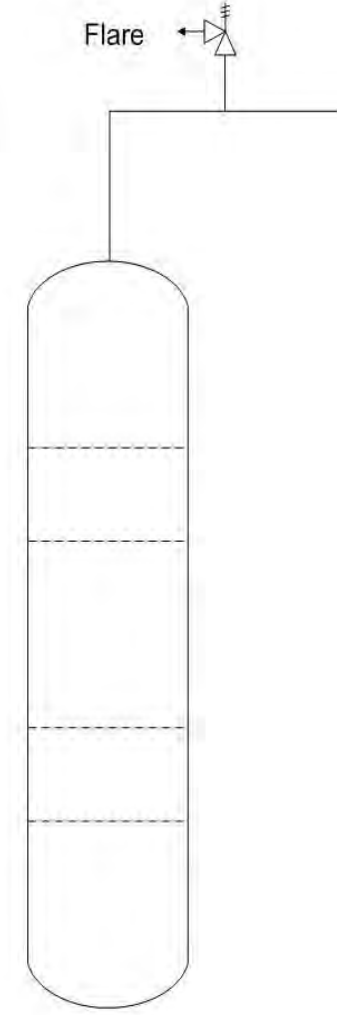
"CLOSE"

Design
SIL-interlock



"CLOSE"

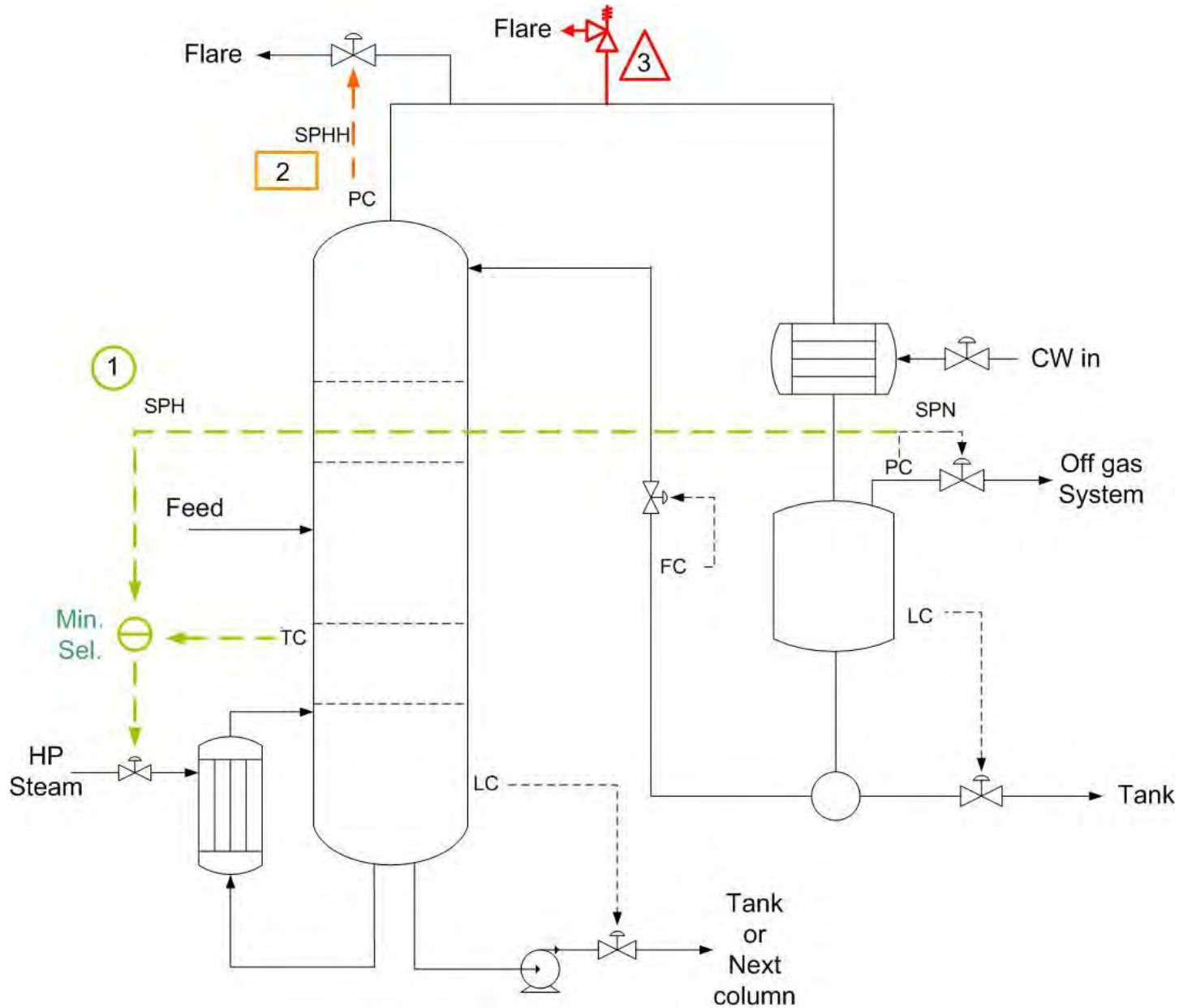
Design
SIL-interlock



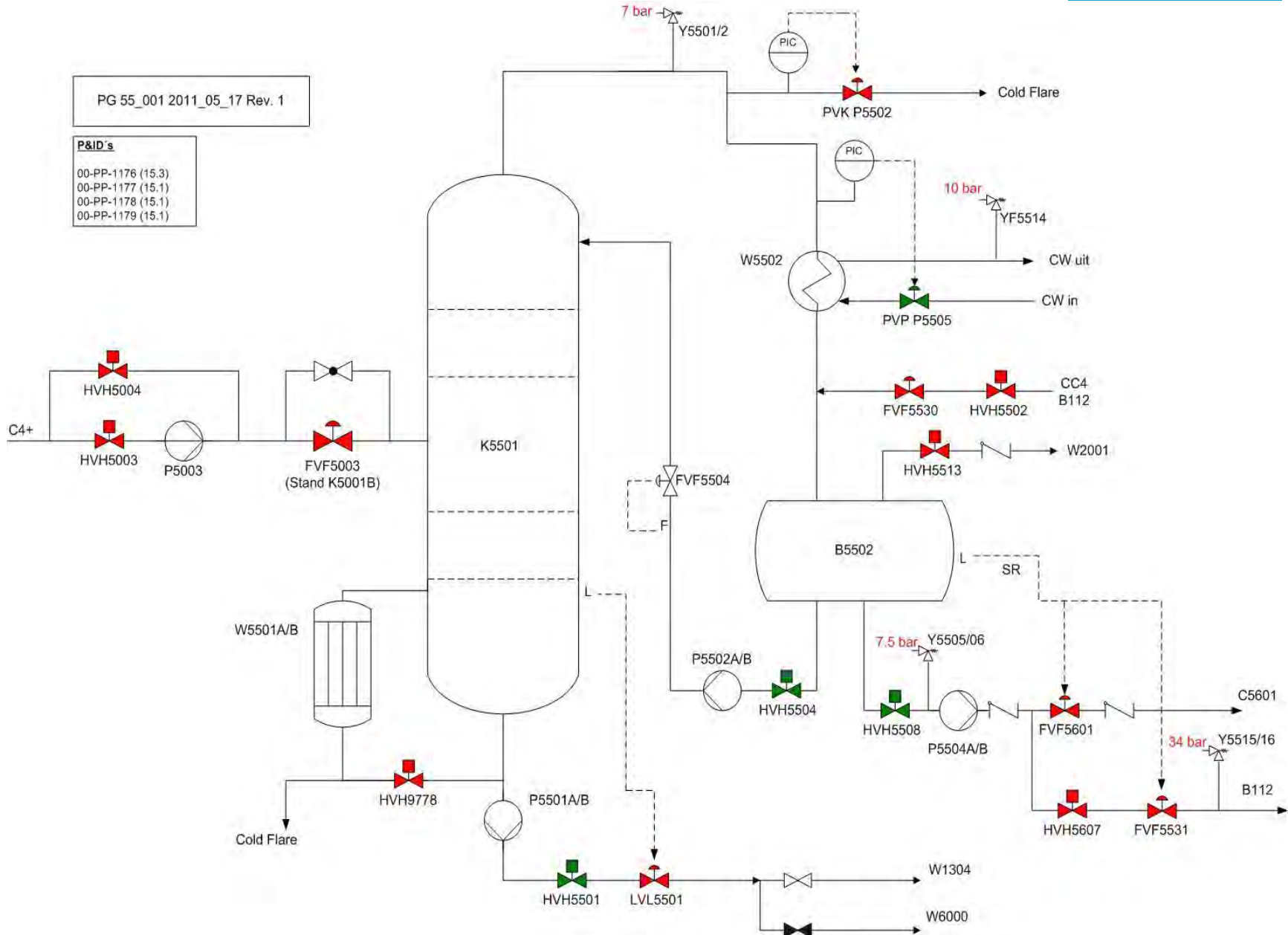
"NA"

Design
Intrinsic Safe

Process Safety Concept – Steamcracker (generic)



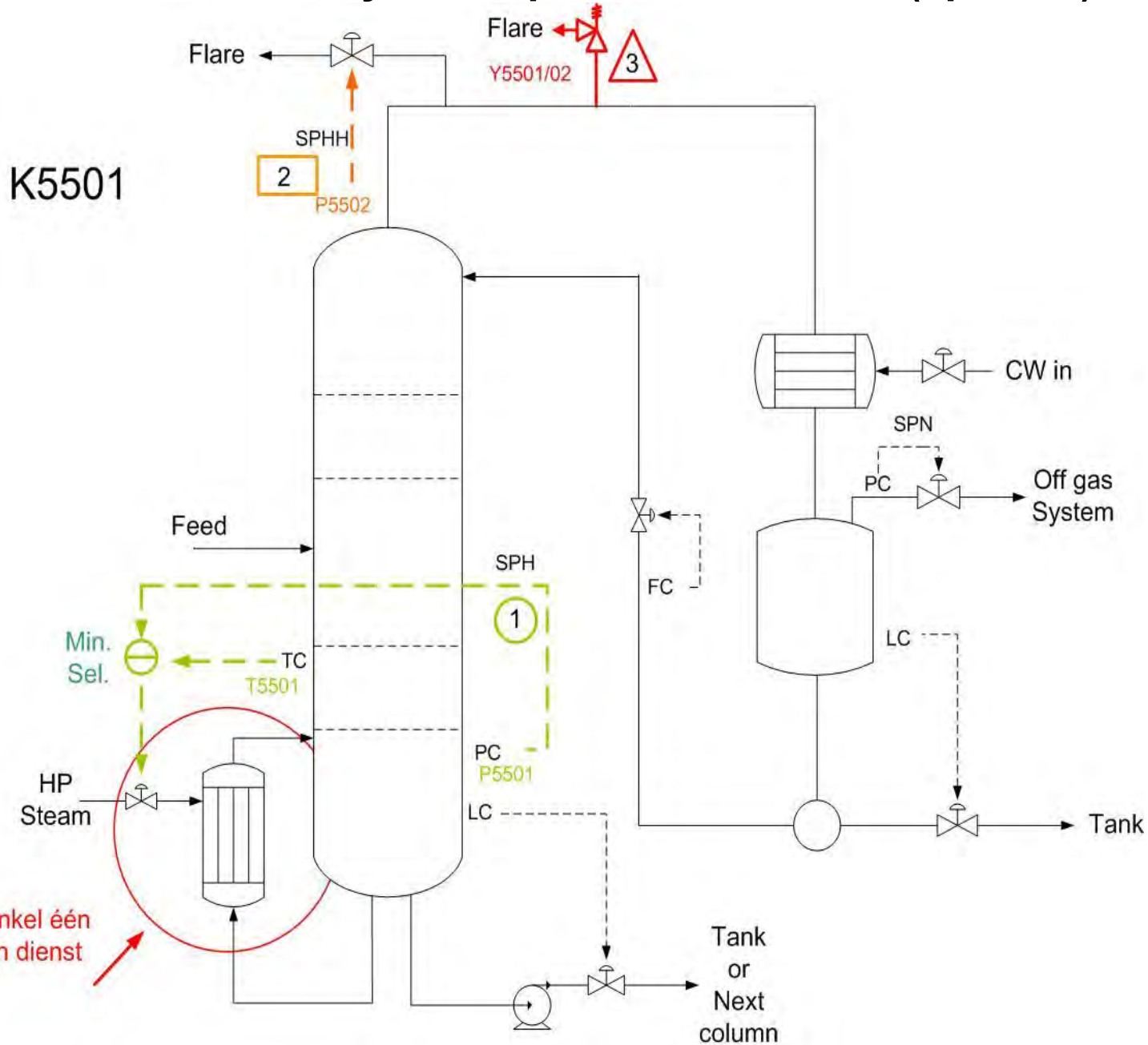
Process Safety Concept – Steamcracker (specific)



PG 55_001 2011_05_17 Rev. 1

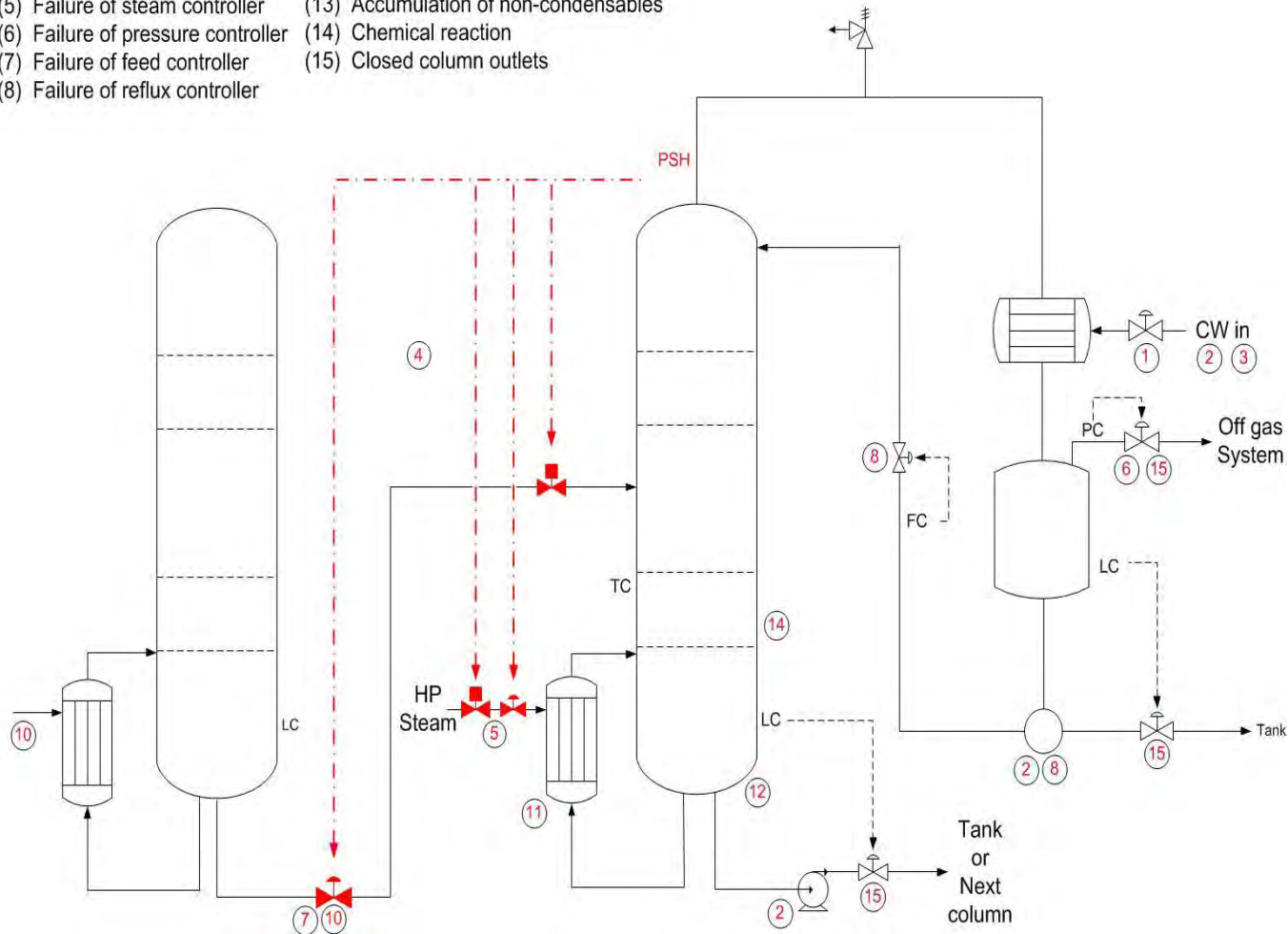
- P&ID's**
- 00-PP-1176 (15.3)
 - 00-PP-1177 (15.1)
 - 00-PP-1178 (15.1)
 - 00-PP-1179 (15.1)

Process Safety Concept – Steamcracker (specific)



Process Safety Concept – Instrumentational

- | | |
|------------------------------------|---|
| (1) Loss of cooling | (9) Valve opening to an external source |
| (2) Loss of power | (10) Loss of heating upstream column |
| (3) Loss of steam | (11) Failure of exchanger |
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Feedback Operators

- Advantages of further in-depth training:
 - Useful for panel operator – broader knowledge of scenarios.
 - Better understanding of limitations installed in the plant (orifices, locked valves, key arrangements, etc.)
 - Schematic diagram, only focusing on safety concept.
- Disadvantages :
 - Too short.
- Higher engagement
 - Questions / E-mails from operators for a variety of themes.



BACK UP

HOW? *To be continued*

- What are the deliverables from the organization during PHA:
 - Roles and responsibilities clearly defined by OPAL-project.
 - Will add extra dimension to validation and quality of risk assessment
 - Move from “Project PHA” to “Life Cycle PHA”

- Foresee in-depth training for each role – combined effort by LPP / PTQ / PTP – see overview

How / to be ctd ... necessary competencys

Global Organisation

Plant Organisation

Site Organisation

Technology Group
PU/T, PB/U, ...

Operations Manager

Inspection PTQ

Safety LP

Production Manager

Process Manager

Asset Manager

Experience exchange with similar units within BASF

Overview incidents similar units extern BASF

New Safety concepts

PID's - FUP's	PFD's - PID's	Technical Documentation
Operation Manual	Overview Scenarios	Maint. Plan
Start up & Shutdown	MOC Safety Assessment	Test freq. & reports
Competency Management	Proj. Safety Assessment	SAP History

Inspection plan

Inspection reports

Expertise (e.g. corrosion)

Legal obligations

BASF corporate guidelines

Expertise (e.g. relevant Incidents)



Questions